

**Section 10**

PROCEDURES MANUAL FOR HAZARDOUS LIQUIDS PIPELINE OPERATIONS,  
MAINTENANCE, AND EMERGENCIES

*Miscellaneous Operating Procedures*

<b>Subject:</b> Pipeline Taps and Branch Connections	<b>Section:</b> 1310
<b>References:</b> ASME B31.4 (current edition), and ASME B1.20.1 (current edition)	<b>Page</b> 1 of 2 <b>Date:</b> 10/31/2009

**Scope:**

The procedures prescribe the actions taken to safely install pipeline taps and branch connections.

**Procedure:**

Hot tapping is the method for welding a branch connection onto a pipeline that is under pressure and in service for the purpose of cutting an opening in the line. While hot tapping is recognized as an important tool in industry, there are certain inherent risks involved. For this reason, hot tapping is not a routine procedure and should be limited to those situations where there is a necessity for the hot tap.

Each hot tap will be treated as a special case and a Hot Tap Procedure and a Hot Tap "assessment letter" for the job will be issued. Engineering is responsible for the assessment of all hot taps to determine the technical feasibility of performing a hot tap in accordance with the Company Engineering specifications. This includes mechanical inspections, review of process conditions, calculations and an overview of all requirements and considerations.

A crew qualified to make hot taps shall perform each tap made on a pipeline under pressure. Each tap or welded branch connection shall be designed and reinforced so that the strength of the pipeline system is not reduced, taking into account the stress in the remaining pipe wall due to the opening in the pipe or header, the shear stress produced by the pressure acting on the area of the branch opening, and any external loading due to thermal movement, weight, and vibration. Each mechanical fitting used to make a hot tap shall be designed for at least the design pressure of the pipeline. Reinforcement of branch connections shall be in accordance with ANSI B31.4 and API 2201.

Industry and vendor procedures for threaded connections, and other connections shall be followed in conjunction with proper pipeline design and alignment procedures. Threaded connections are to be manufactured and installed in accordance with ASME B1.20.1.

**Responsibilities:**

Area Supervision shall be responsible for seeing that the prescribed procedures are complied with and the required records are prepared and filed.

**Records:**

A record shall be made of each hot tap or branch connection installed on a pipeline. Records shall be retained in the Liquids Integrity Group, Records/Data/GIS Group, and/or Project Engineering Group for the life of the pipeline.

Records Retention information is located in the EPCO Records Retention

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	<b>Date:</b> 10/31/2009

Schedule available through the EPCO Internet Portal.

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## Section 11

AN AMERICAN NATIONAL STANDARD

# PIPE THREADS, GENERAL PURPOSE (INCH)

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ANSI/ASME B1.20.1 - 1983

(REVISION AND REDESIGNATION OF ANSI B2.1-1968)

**REAFFIRMED 1992**

FOR CURRENT COMMITTEE PERSONNEL  
PLEASE SEE ASME MANUAL AS-11

**REAFFIRMED 2001**

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## FOREWORD

(This Foreword is not part of American National Standard, Pipe Threads, General Purpose (Inch) ANSI/ASME B1.20.1-1983.)

In 1973 American National Standards Committee B2, which had formerly been responsible for pipe thread standards, was absorbed by ANSI Standards Committee B1 and reorganized as subcommittee 20. A complete rewrite of the B2.2-1968 standard on Dryseal Pipe Threads has been completed, with the product thread data in separate documents from the gaging standards for Dryseal Pipe Threads. The system of numbering, to include metric conversions, is as follows:

ANSI B1.20.3-1976 Dryseal Pipe Threads (Inch)  
ANSI B1.20.4-1976 Dryseal Pipe Threads (Metric Translation)  
ANSI B1.20.5-1978 Gaging for Dryseal Pipe Threads (Inch)  
In preparation, B1.20.6M Gaging for Dryseal Pipe Threads (Metric Translation)

A complete rewrite of the B2.1-1968 standard on Pipe Threads (Except Dryseal) was then undertaken. The system of numbering, to include metric conversions, is as follows:

ANSI/ASME B1.20.1 Pipe Threads, General Purpose (Inch)  
In preparation, B1.20.2M Pipe Threads, General Purpose (Metric Translation)

These standards, ANSI/ASME B1.20.1 and B1.20.2M, have product thread dimensions and gaging in the same document. Thread inspection specifies the use of  $L_1$  taper thread plug and ring gages similar to B2.1-1968. In addition, emphasis is given to the requirement that all basic thread design dimensions are to be met within the specified tolerances.

The data in this Standard supersede those given in ANSI B2.1-1968.

The ANSI/ASME B1.20.1 was approved by ASME Standards Committee B1 on December 1, 1982 for publication as an official ANSI standard.

The proposed standard was submitted by standards committee B1 to the Secretariat and the American National Standards Institute. It was approved and formally designated as an American National Standard on February 4, 1983.



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AN AMERICAN NATIONAL STANDARD  
PIPE THREADS, GENERAL PURPOSE (INCH)

## 1 INTRODUCTION

### 1.1 Scope

This American National Standard covers dimensions and gaging of pipe threads for general purpose applications.

### 1.2 Thread Designations

1.2.1 The types of pipe threads included in this Standard are designated by specifying in sequence the nominal pipe size,<sup>1</sup> number of threads per inch and the thread series symbol as follows:

3/8 - 18 NPT  
1/8 - 27 NPSC  
1/2 - 14 NPTR  
1/8 - 27 NPSM  
1/8 - 27 NPSL  
1 - 11.5 NPSH

For left hand threads add LH to the designation, otherwise right hand threads will be understood. For example:

3/8 - 18 NPT - LH

1.2.2 Each of these letters in the symbols has a definite significance as follows:

N = National (American) Standard  
P = Pipe  
T = Taper  
C = Coupling  
S = Straight  
M = Mechanical  
L = Locknut  
H = Hose Coupling  
R = Railing Fittings

<sup>1</sup>Where it is necessary to use decimal notation for the size designation (as when inserting such in a computer or electronic accounting machine) the decimal equivalent of nominal pipe size may be substituted for fractional pipe sizes.

1.2.3 Coated or Plated Threads. The threaded product specifications covered in this Standard do not include an allowance for coatings or plating.

### 1.3 Sealing

1.3.1 Where pressure-tight joints are required, it is intended that taper pipe threads conforming to this Standard be made up wrench-tight with a sealant. To prevent galling on certain piping materials such as stainless steels, the sealant usually contains a lubricant.

1.3.2 Pipe threads designed for pressure-tight joints that may be used without sealing compounds (Dryseal Threads) are covered in ANSI B1.20.3 (Inch) and ANSI B1.20.4 (Metric Translation).

### 1.4 Inspection

A gaging method and tolerances are prescribed in this Standard to effect a functional inspection of the handtight  $L_1$  engagement threads. However, conformance to this Standard requires that all basic design dimensions be met (within applicable tolerances) including extension of the thread elements to provide for wrench-tight makeup. Therefore, additional methods of gaging may be employed to evaluate conformance to the basic design dimensions. When additional methods of gaging are employed, they shall be agreed upon by the supplier and the purchaser.

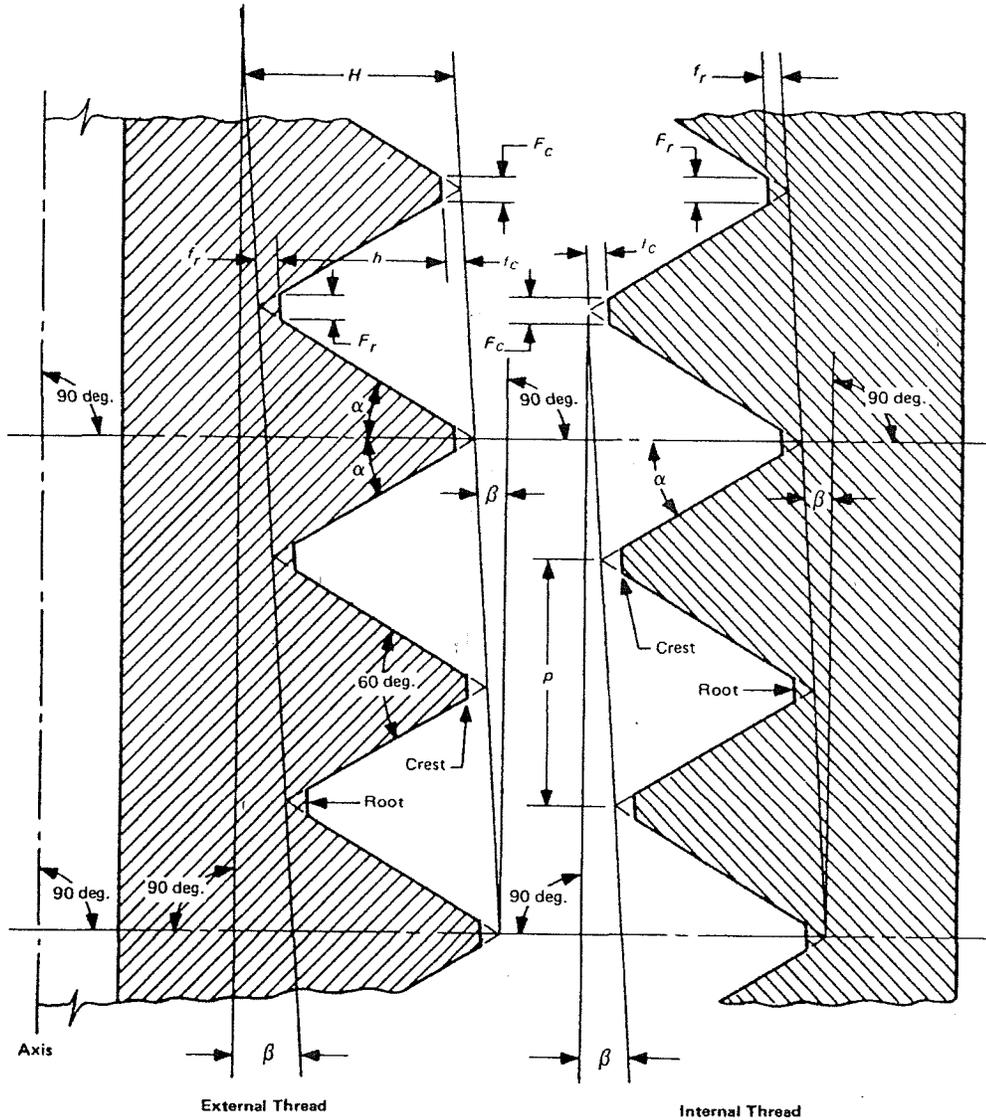
### 1.5 Appendix

Useful and supplementary information which is not a part of this Standard is presented in the Appendix. Specifically, the Appendix gives Suggested Twist Drill Diameters for Drilled Hole Sizes for Pipe Threads.

### 1.6 Related Standard

Definitions of terms and symbols for thread dimensions are given in ANSI B1.7, Nomenclature, Definitions and Letter Symbols for Screw Threads.





NOTATION

- |  |   |
|--|---|
| $H = 0.866025p$ = height of 60 deg. sharp V thread | $\beta = 1 \text{ deg. } 47 \text{ min.}$ = thread taper angle for 1/16 taper |
| $h = 0.800000p$ = height of thread on product      | $f_c$ = depth of truncation at crest  |
| $p = 1/n$ = pitch (measured parallel to axis)      | $f_r$ = depth of truncation at root   |
| $n$ = number of threads per inch                   | $F_c$ = width of flat at crest  |
| $\alpha = 30 \text{ deg.}$ = thread flank angle    | $F_r$ = width of flat at root   |

GENERAL NOTE: For a symmetrical straight screw thread,  $H = \cot \alpha / 2n$ . For a symmetrical taper screw thread,  $H = (\cot \alpha - \tan^2 \beta \tan \alpha) / 2n$ , so that the exact value for an American National Standard taper pipe thread is  $H = 0.865743p$  as against  $H = 0.866025p$ , the value given above. For an 8-pitch thread, which is the coarsest standard taper pipe thread pitch, the corresponding values of  $H$  are 0.108218 and 0.108253 respectively, the difference being 0.000035 inch. This difference being too small to be significant, the value of  $H = 0.866025p$  continues in use for threads of 0.750 in., or less, taper/ft on the diameter.

FIG. 1 BASIC FORM OF AMERICAN NATIONAL STANDARD TAPER PIPE THREAD

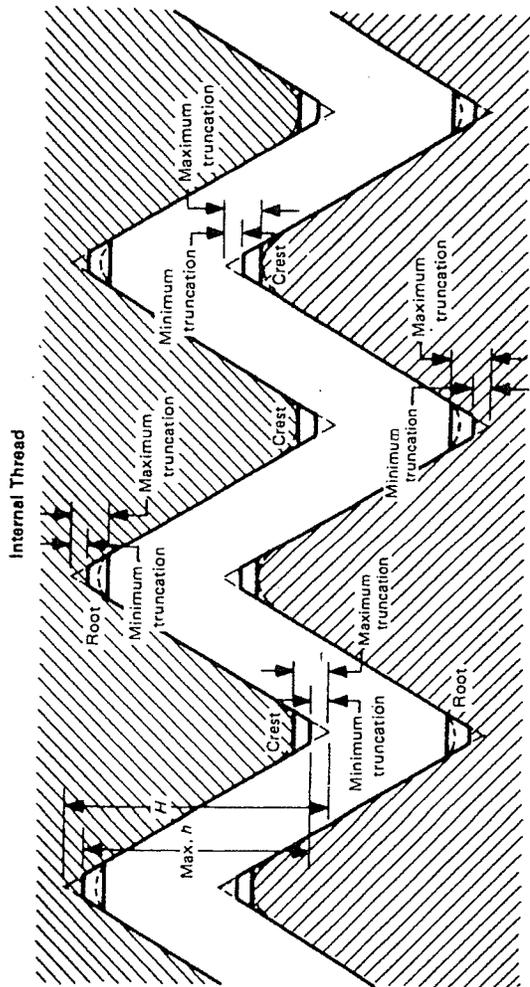
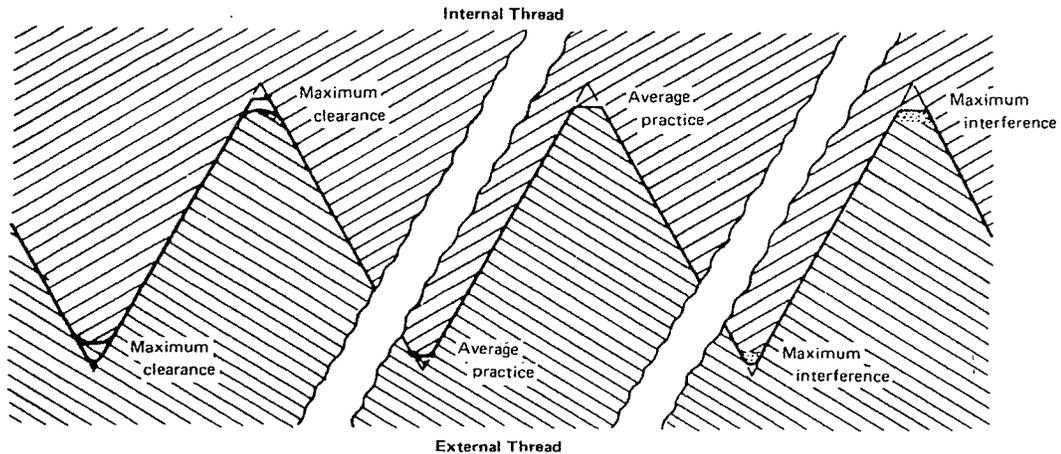


TABLE 1 LIMITS ON CREST AND ROOT TRUNCATION OF AMERICAN NATIONAL STANDARD EXTERNAL AND INTERNAL TAPER PIPE THREADS, NPT<sup>1</sup>

Threads/ in. (n)	Height of Sharp V Thread (H)		Height of Thread (h)		Truncation (f)						Equivalent Width of Flat (F)			
	Maximum	Minimum	Maximum	Minimum	Minimum		Maximum		Tolerance		Minimum		Maximum	
					Formula	in.	Formula	in.	Formula	in.	Formula	in.	Formula	in.
1	2	3	4	5	6	7	8	9	10	11	12	13	14	
27	0.03208	0.02963	0.02496	0.033p	0.0012	0.096p	0.0036	0.0024	0.038p	0.0014	0.111p	0.0041	0.0027	
18	0.04811	0.04444	0.03833	0.033p	0.0018	0.088p	0.0049	0.0031	0.038p	0.0021	0.102p	0.0057	0.0036	
14	0.06186	0.05714	0.05071	0.033p	0.0024	0.078p	0.0056	0.0032	0.038p	0.0027	0.090p	0.0064	0.0037	
11.5	0.07531	0.06957	0.06261	0.033p	0.0029	0.073p	0.0063	0.0034	0.038p	0.0033	0.084p	0.0073	0.0040	
8	0.10825	0.10000	0.09275	0.033p	0.0041	0.062p	0.0078	0.0037	0.038p	0.0048	0.072p	0.0090	0.0042	

NOTE:

(1) The basic dimensions of the American National Standard Taper Pipe Thread are given in inches to four and five decimal places. While this implies a greater degree of precision than is ordinarily attained, these dimensions are so expressed for the purpose of eliminating errors in computations.



**GENERAL NOTE:**

When threaded joints are made up wrench-tight with lubricant or sealer, it is intended that the flanks shall be in contact.

**FIG. 2. AMERICAN NATIONAL STANDARD TAPER PIPE THREADS FOR PRESSURE-TIGHT JOINTS, NPT**

**2 AMERICAN NATIONAL STANDARD  
PIPE THREAD FORM**

$$h = 0.800p = 0.800/n$$

**2.1 Thread Form**

The form of thread profile specified in this Standard shall be known as the American National Standard Pipe Thread Form. The relations as specified herein, for form of thread and general notation are shown in Fig. 1.

**2.2 Angle of Thread**

The angle between the sides of the thread is 60 deg when measured in an axial plane. The line bisecting this angle is perpendicular to the axis.

**2.3 Truncation and Thread Height**

The height of the sharp *V* thread, *H*, is

$$H = 0.866025p = 0.866025/n$$

where

*p* = pitch of thread  
*n* = threads per inch

The basic maximum depth of the truncated thread, *h* (see Fig. 1), is based on factors entering into the manufacture of cutting tools and the making of tight joints.

The crest and root of pipe threads are truncated a minimum of  $0.033p$ . The maximum depth of truncation for the crest and root of these pipe threads will be found in Table 1. The crests and roots of the external and internal threads may be truncated either parallel to the pitch line or parallel to the axis.

The sketch in Table 2, giving a sectional view of this Standard thread form, represents the truncated thread form by a straight line. However, when closely examined, the crests and roots of commercially manufactured pipe threads appear slightly rounded. When crests and roots of threading tools or chasers lie within the limits shown in Table 1, the pipe threads of products produced by such means are acceptable on the basis of in-process control.

**3 SPECIFICATION FOR GENERAL PURPOSE  
TAPER PIPE THREADS, NPT**

**3.1 Taper Pipe Threads**

Threads made in accordance with these specifications consist of an external taper and an internal taper thread, to form the normal type of joint having general application on pipe and fittings. See Fig. 2.

NPT taper pipe threads are intended to be made up wrench-tight and with a sealant whenever a pressure-tight joint is required.

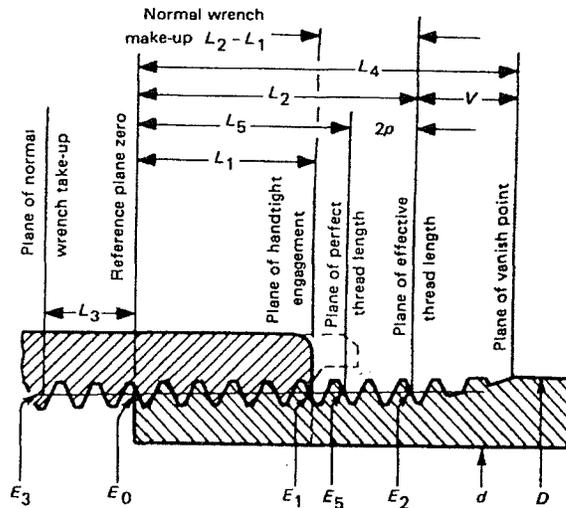


FIG. 3 AMERICAN NATIONAL STANDARD  
TAPER PIPE THREAD NOTATION

Sealing is affected by out-of-roundness which is possible between the wrench-tight mated parts in final assembly. This will vary depending on the method for producing the thread in conjunction with the elasticity and/or ductility of the mating parts and the resultant conformance at final assembly.

**3.1.1 Thread Designation and Notation.** American National Standard Taper Pipe Threads are designated in accordance with 1.2.1 as follows:

3/8 - 18 NPT

Standard notation applicable to American National Standard Taper Pipe Threads is shown in Fig. 3.

**3.1.2 Designation of Plated Threads.** The product specifications of this Standard do not include an allowance for plating. If plating is desired, it may be necessary to modify the threads since the same final gaging requirements must be satisfied for plated and unplated parts. This may be emphasized by adding the words AFTER PLATING to the designation. For manufacturing purposes, notes for plated taper pipe threads may specify the gage limits (turns or threads engagement) before plating followed by the words BEFORE PLATING. These should be followed by the standard gage limits (turns or threads engagement) after plating and the words AFTER PLATING.

**3.1.3 Form of Thread.** The form of the thread for American National Standard Taper Pipe Threads is that specified in 2.1.

**3.1.4 Taper of Thread.** The taper of the thread is 1 in 16 or 0.75 in./ft measured on the diameter and along the axis.

**3.1.5 Diameter of Thread.** The basic pitch diameters of the taper thread are determined by the following formulas<sup>2</sup> based on the outside diameter of the pipe and the pitch of the thread:

$$E_0 = D - (0.05D + 1.1) 1/n$$

$$= D - (0.05D + 1.1) p$$

$$E_1 = E_0 + 0.0625L_1$$

where

$D$  = outside diameter of pipe

$E_0$  = pitch diameter of thread at end of pipe or small end of external thread

$E_1$  = pitch diameter of thread at the gaging notch or large end of internal thread

$L_1$  = normal engagement by hand between external and internal threads

$n$  = threads per inch

<sup>2</sup>For the 1/8-27 and 1/4-18 sizes,  $E_1$  approx. =  $D - (0.05D + 0.827) p$ .



AN AMERICAN NATIONAL STANDARD  
PIPE THREADS, GENERAL PURPOSE (INCH)

ANSI/ASME B1.20.1-1983

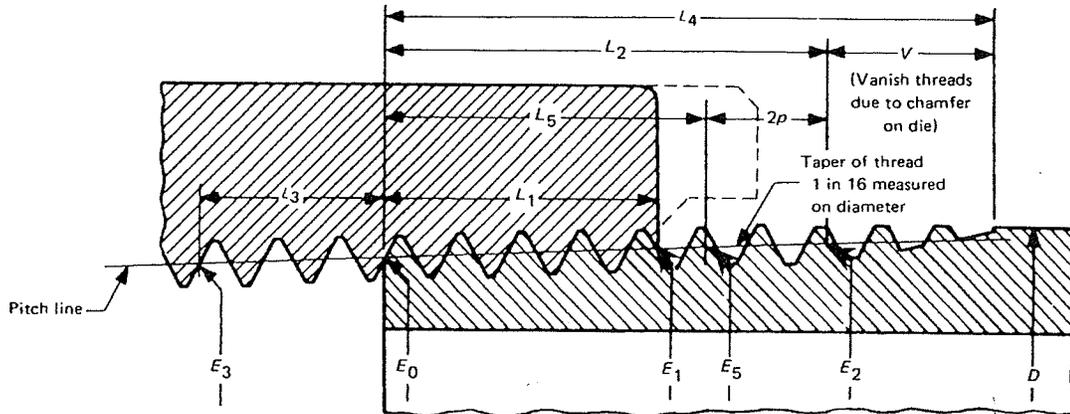


TABLE 2 BASIC DIMENSIONS OF AMERICAN NATIONAL STANDARD TAPER PIPE THREAD, NPT<sup>1</sup>

Nominal Pipe Size	O.D. of Pipe (D)	Threads/in. (n)	Pitch of Thread (P)	Pitch Diam. at Beginning of External Thread (E <sub>0</sub> )	Handtight Engagement			Effective Thread, External		
					Length <sup>2</sup> (L <sub>1</sub> )		Diam. <sup>3</sup> (E <sub>1</sub> )	Length <sup>4</sup> (L <sub>2</sub> )		Diam. (E <sub>2</sub> )
					inch	Threads		inch	Threads	
1	2	3	4	5	6	7	8	9	10	11
1/16	0.3125	27	0.03704	0.27118	0.160	4.32	0.28118	0.2611	7.05	0.28750
1/8	0.405	27	0.03704	0.36351	0.1615	4.36	0.37360	0.2639	7.12	0.38000
1/4	0.540	18	0.05556	0.47739	0.2278	4.10	0.49163	0.4018	7.23	0.50250
3/8	0.675	18	0.05556	0.61201	0.240	4.32	0.62701	0.4078	7.34	0.63750
1/2	0.840	14	0.07143	0.75843	0.320	4.48	0.77843	0.5337	7.47	0.79179
3/4	1.050	14	0.07143	0.96768	0.339	4.75	0.98887	0.5457	7.64	1.00179
1	1.315	11.5	0.08696	1.21363	0.400	4.60	1.23863	0.6828	7.85	1.25630
1 1/4	1.660	11.5	0.08686	1.55713	0.420	4.83	1.58338	0.7068	8.13	1.60130
1 1/2	1.900	11.5	0.08696	1.79609	0.420	4.83	1.82234	0.7235	8.32	1.84130
2	2.375	11.5	0.08696	2.26902	0.436	5.01	2.29627	0.7565	8.70	2.31630
2 1/2	2.875	8	0.12500	2.71953	0.682	5.46	2.76216	1.1375	9.10	2.79062
3	3.500	8	0.12500	3.34062	0.766	6.13	3.38850	1.2000	9.60	3.41562
3 1/2	4.000	8	0.12500	3.83750	0.821	6.57	3.88881	1.2500	10.00	3.91562
4	4.500	8	0.12500	4.33438	0.844	6.75	4.38712	1.3000	10.40	4.41562
5	5.563	8	0.12500	5.39073	0.937	7.50	5.44929	1.4063	11.25	5.47862
6	6.625	8	0.12500	6.44609	0.958	7.66	6.50597	1.5125	12.10	6.54062
8	8.625	8	0.12500	8.43359	1.063	8.50	8.50003	1.7125	13.70	8.54062
10	10.750	8	0.12500	10.54531	1.210	9.68	10.62094	1.9250	15.40	10.66562
12	12.750	8	0.12500	12.53281	1.360	10.88	12.61781	2.1250	17.00	12.66562
14 O.D.	14.000	8	0.12500	13.77500	1.562	12.50	13.87262	2.2500	18.00	13.91562
16 O.D.	16.000	8	0.12500	15.76250	1.812	14.50	15.87575	2.4500	19.60	15.91562
18 O.D.	18.000	8	0.12500	17.75000	2.000	16.00	17.87500	2.6500	21.20	17.91562
20 O.D.	20.000	8	0.12500	19.73750	2.125	17.00	19.87031	2.8500	22.80	19.91562
24 O.D.	24.000	8	0.12500	23.71250	2.375	19.00	23.86094	3.2500	26.00	23.91562

NOTES:

- (1) The basic dimensions of the American National Standard Taper Pipe Thread are given in inches to four or five decimal places. While this implies a greater degree of precision than is ordinarily attained, these dimensions are the basis of gage dimensions and are so expressed for the purpose of eliminating errors in computations.
- (2) Also length of thin ring gage and length from gaging notch to small end of plug gage.
- (3) Also pitch diameter at gaging notch (handtight plane).
- (4) Also length of plug gage.

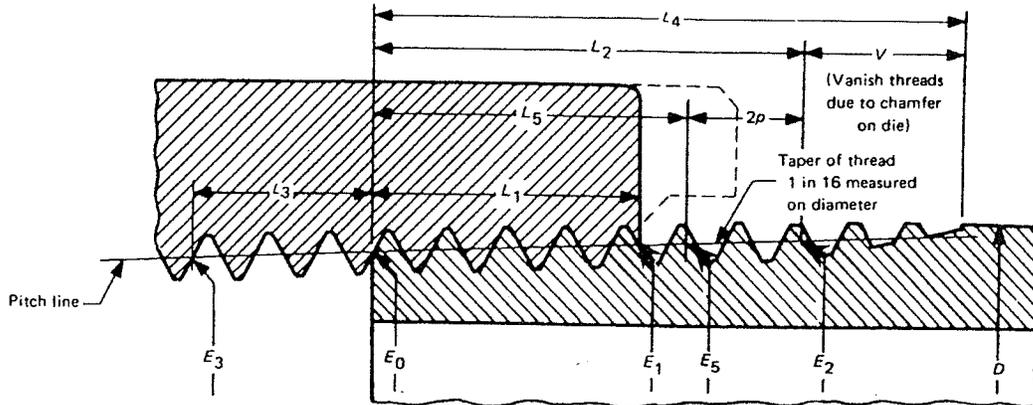


TABLE 2 BASIC DIMENSIONS OF AMERICAN NATIONAL STANDARD TAPER PIPE THREAD, NPT<sup>1</sup> (CONT'D)

Nominal Pipe Size	Length, $L_1$ Plane to $L_2$ Plane External Thread ( $L_2 - L_1$ )		Wrench Makeup Length for Internal Thread <sup>7</sup>		Diam. ( $E_3$ )	Vanish Thread ( $V$ )		Overall <sup>8</sup> Length External Thread ( $L_4$ )	Nominal Complete External Threads <sup>5</sup>		Height of Thread ( $h$ )	Increase in Diam./Thread (0.0625/ $n$ )	Basic <sup>6</sup> Minor Diam. at Small End of Pipe ( $K_0$ )
	in.	Thread	in.	Thread		in.	Thread		Length ( $L_5$ )	Diam. ( $E_5$ )			
1	12	13	14	15	16	17	18	19	20	21	22	23	24
1/16	0.1011	2.73	0.1111	3	0.26424	0.1285	3.47	0.3896	0.1870	0.28287	0.02963	0.00231	0.2416
1/8	0.1024	2.76	0.1111	3	0.35656	0.1285	3.47	0.3924	0.1898	0.37537	0.02963	0.00231	0.3339
1/4	0.1740	3.13	0.1667	3	0.46697	0.1928	3.47	0.5946	0.2907	0.49556	0.04444	0.00347	0.4329
3/8	0.1678	3.02	0.1667	3	0.60160	0.1928	3.47	0.6006	0.2967	0.63056	0.04444	0.00347	0.5676
1/2	0.2137	2.99	0.2143	3	0.74504	0.2478	3.47	0.7815	0.3909	0.78286	0.05714	0.00446	0.7013
3/4	0.2067	2.89	0.2143	3	0.95429	0.2478	3.47	0.7935	0.4029	0.99286	0.05714	0.00446	0.9105
1	0.2828	3.25	0.2609	3	1.19733	0.3017	3.47	0.9845	0.5089	1.24543	0.06957	0.00543	1.1441
1 1/4	0.2868	3.30	0.2609	3	1.54083	0.3017	3.47	1.0085	0.5329	1.59043	0.06957	0.00543	1.4876
1 1/2	0.3035	3.49	0.2609	3	1.77978	0.3017	3.47	1.0252	0.5496	1.83043	0.06957	0.00543	1.7265
2	0.3205	3.69	0.2609	3	2.25272	0.3017	3.47	1.0582	0.5826	2.30543	0.06957	0.00543	2.1995
2 1/2	0.4555	3.64	0.2500	2	2.70391	0.4337	3.47	1.5712	0.8875	2.77500	0.100000	0.00781	2.6195
3	0.4340	3.47	0.2500	2	3.32500	0.4337	3.47	1.6337	0.9500	3.40000	0.100000	0.00781	3.2406
3 1/2	0.4290	3.43	0.2500	2	3.82188	0.4337	3.47	1.6837	1.0000	3.90000	0.100000	0.00781	3.7375
4	0.4560	3.65	0.2500	2	4.31875	0.4337	3.47	1.7337	1.0500	4.40000	0.100000	0.00781	4.2344
5	0.4693	3.75	0.2500	2	5.37511	0.4337	3.47	1.8400	1.1563	5.46300	0.100000	0.00781	5.2907
6	0.5545	4.44	0.2500	2	6.43047	0.4337	3.47	1.9462	1.2625	6.52500	0.100000	0.00781	6.3461
8	0.6495	5.20	0.2500	2	8.41797	0.4337	3.47	2.1462	1.4625	8.52500	0.100000	0.00781	8.3336
10	0.7150	5.72	0.2500	2	10.52969	0.4337	3.47	2.3587	1.6750	10.65000	0.100000	0.00781	10.4453
12	0.7650	6.12	0.2500	2	12.51719	0.4337	3.47	2.5587	1.8750	12.65000	0.100000	0.00781	12.4328
14 O.D.	0.6880	5.50	0.2500	2	13.75938	0.4337	3.47	2.6837	2.0000	13.90000	0.100000	0.00781	13.6750
16 O.D.	0.6380	5.10	0.2500	2	15.74688	0.4337	3.47	2.8837	2.2000	15.90000	0.100000	0.00781	15.6625
18 O.D.	0.6500	5.20	0.2500	2	17.73438	0.4337	3.47	3.0837	2.4000	17.90000	0.100000	0.00781	17.6500
20 O.D.	0.7250	5.80	0.2500	2	19.72188	0.4337	3.47	3.2837	2.6000	19.90000	0.100000	0.00781	19.6375
24 O.D.	0.8750	7.00	0.2500	2	23.69688	0.4337	3.47	3.6837	3.0000	23.90000	0.100000	0.00781	23.6125

- (5) The length  $L_5$  from the end of the pipe determines the plane beyond which the thread form is incomplete at the crest. The next two threads are complete at the root. At this plane the cone formed by the crests of the thread intersects the cylinder forming the external surface of the pipe.  $L_5 = L_2 - 2p$ .
- (6) Given as information for use in selecting tap drills. (See Appendix).
- (7) Military Specification MIL-P-7105 gives the wrench makeup as three threads for sizes 3 and smaller. The  $E_3$  dimensions are as follows: Nominal pipe size 2 1/2 = 2.69609 and size 3 = 3.31719; sizes 2 and smaller same as above, col. 16.
- (8) Reference dimension.

TABLE 3 TOLERANCES ON TAPER, LEAD, AND  
ANGLE OF PIPE THREADS, NPT

Nominal Pipe Size	Threads/in. (n)	Tolerances			60 deg. Angle of Threads, degrees (±)
		Taper on Pitch Line (3/4 in./ft)		Lead in Length of Effective Threads (±)	
		Maximum	Minimum		
1	2	3	4	5	6
1/16, 1/8	27	+ 1/8	- 1/16	0.003	2 1/2
1/4, 3/8	18	+ 1/8	- 1/16	0.003	2
1/2, 3/4	14	+ 1/8	- 1/16	0.003 <sup>1</sup>	2
1, 1 1/4, 1 1/2, 2	11.5	+ 1/8	- 1/16	0.003 <sup>1</sup>	1 1/2
2 1/2 and larger	8	+ 1/8	- 1/16	0.003 <sup>1</sup>	1 1/2

GENERAL NOTE:

For tolerances on depth of thread see Table 1, and for tolerances on functional size, see 3.2.1.

NOTE:

(1) The tolerance on lead shall be ±0.003 in./in. on any size threaded to an effective thread length greater than 1 in.

TABLE 4 DIMENSIONS, INTERNAL STRAIGHT THREADS IN PIPE COUPLING, NPS  
(Pressure-tight Joints With Lubricant or Sealant)

Nominal Pipe Size	O.D. of Pipe (D)	Threads/in. (n)	Minor Diameter, Minimum	Pitch Diameter <sup>1</sup>	
				Minimum	Maximum
1	2	3	4	5	6
1/8	0.405	27	0.340	0.3701	0.3771
1/4	0.540	18	0.442	0.4864	0.4968
3/8	0.675	18	0.577	0.6218	0.6322
1/2	0.840	14	0.715	0.7717	0.7851
3/4	1.050	14	0.925	0.9822	0.9956
1	1.315	11.5	1.161	1.2305	1.2468
1 1/4	1.660	11.5	1.506	1.5752	1.5915
1 1/2	1.900	11.5	1.745	1.8142	1.8305
2	2.375	11.5	2.219	2.2881	2.3044
2 1/2	2.875	8	2.650	2.7504	2.7739
3	3.500	8	3.277	3.3768	3.4002
3 1/2	4.000	8	3.777	3.8771	3.9005
4	4.500	8	4.275	4.3754	4.3988

NOTE:

(1) Attention is called to the fact that the actual pitch diameter of the straight tapped hole will be slightly smaller than the value given when gaged with a taper plug gage as specified in 9.1.2.

**3.1.6 Length of Thread.** The basic length of the effective external taper thread  $L_2$ , is determined by the following formula based on the outside diameter of the pipe and the pitch of the thread:

$$\begin{aligned} L_2 &= (0.80D + 6.8) 1/n \\ &= (0.80D + 6.8) p \end{aligned}$$

where

$D$  = outside diameter of pipe  
 $n$  = threads per inch

This formula determines directly the length of effective thread which includes two usable threads slightly incomplete at the crest.

**3.1.7 Engagement Between External and Internal Taper Threads.** The normal length of engagement between external and internal taper threads when screwed together handtight is shown in col. 6, Table 2. This length is controlled by the construction and use of the gages. It is recognized that in special applications, such as flanges for high pressure work, longer thread engagement is used, in which case the pitch diameter (dimension  $E_1$ , Table 2) is maintained and the pitch diameter  $E_0$  at the end of the pipe is proportionately smaller.

**3.1.8 Basic Dimensions.** The basic dimensions of taper pipe threads, derived from the above specifications, are given in Table 2. All dimensions are given in inches unless otherwise specified.

### 3.2 Tolerances

**3.2.1 Manufacturing Tolerance on Product.** The maximum allowable deviation in the commercial product is one turn large or small from gages made to the basic dimensions. See 8.2 and 8.3.

**3.2.2 Tolerances on Thread Elements.** The permissible deviations in thread elements are given in Table 3. This table is a guide for establishing limits of the thread elements of taps, dies, and thread chasers. Conformance to these limits may be required on product threads, in which case specifications shall require control and checking of thread elements.

On pipe fittings and valves (not steel or high grade alloys used in critical services) for steam pressures 300 lb and below, it is intended that plug and ring gage practices as established in this Standard be used

in conjunction with tooling control of thread elements, e.g., taps and dies, to provide satisfactory control of functional size. Therefore, no tolerances on thread elements have been established for this class.

For service conditions, where more exact checks are required, procedures have been developed by industry to supplement the standard plug and ring gage method of gaging.

## 4 SPECIFICATIONS FOR INTERNAL STRAIGHT THREADS IN PIPE COUPLINGS, NPSC

### 4.1 Straight Pipe Threads in Pipe Couplings

Threads in pipe couplings made in accordance with these specifications are straight (parallel) threads of the same thread form as the American National Standard Taper Pipe Thread specified in 2.1. They are used to form pressure-tight joints when assembled with an American National Standard external taper pipe thread and made up wrench-tight with lubricant or sealant.

**4.1.1 Thread Designation.** The American National Standard Coupling Straight Pipe Threads are designated in accordance with 1.2.1 as follows:

1/8 - 27 NPSC

**4.1.2 Dimensions and Limits of Size.** The dimensions and pitch diameter limits of size are specified in Table 4. The pitch diameter limits of size correspond to one and one-half turns large or small of the standard taper pipe thread. The major and minor diameters vary with the pitch diameter, as the American National Standard Pipe Thread form is maintained within the truncation tolerances shown in Table 1.

## 5 SPECIFICATIONS FOR RAILING JOINT TAPER PIPE THREADS, NPTR

### 5.1 Railing Joints

Railing joints that require a rigid mechanical thread joint may be made with external and internal taper threads.

The external thread is basically the same as the American National Standard Taper Pipe Thread, except that it is shortened to permit the use of the



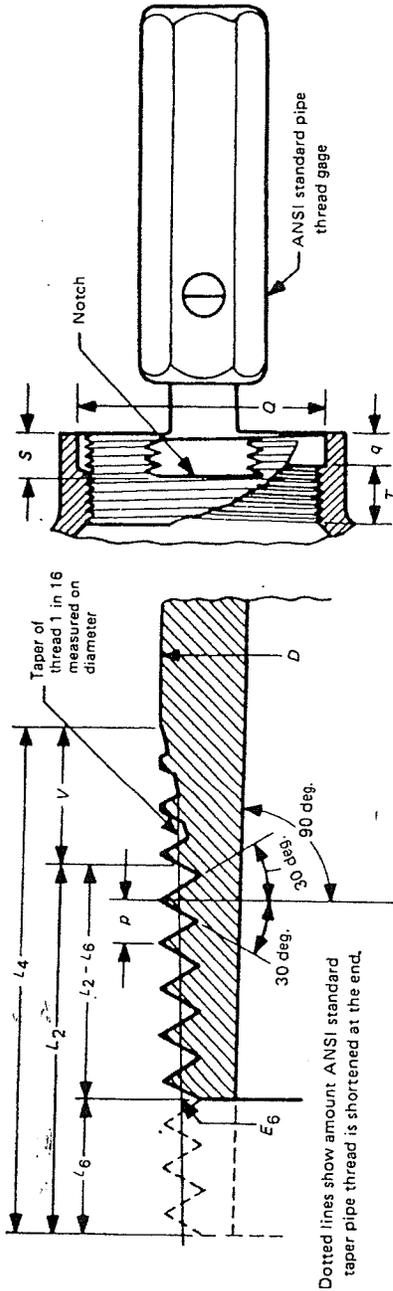


TABLE 5 DIMENSIONS OF EXTERNAL AND INTERNAL TAPER PIPE THREADS FOR RAILING JOINTS, NPTR<sup>1</sup>  
(Mechanical Joints)

Nom. Pipe Size	O.D. of Pipe (D)	Threads/in. (n)	Height of Thread (h)	Pitch Diameter at End of External Thread (E <sub>6</sub> )	Shortening of Thread (L <sub>6</sub> )		Length of Effective Thread (L <sub>2</sub> - L <sub>6</sub> )		Total Length of External Thread, max. (L <sub>4</sub> - L <sub>6</sub> )		Incomplete Threads due to Chamfer of Die, max. (V)		Depth of Recess in Fitting (q)		Dia. of Recess in Fitting (Q)		Length (T)		Distance Gage <sup>2</sup> Notch comes below Face of Fitting (S)
					in.	Threads	in.	Threads	in.	Threads	in.	Threads	Minimum	Threads	Minimum	Threads	Minimum	Threads	
1	2	3	4	5	6	7	8	9	10	11	12	13	14	15	16	17	18		
1/2	0.840	14	0.0571	0.7718	0.214	3	0.320	4.47	0.499	6.98	0.179	2 1/2	0.18	0.86	0.25	0.286	4	0.286	
3/4	1.050	14	0.0571	0.9811	0.214	3	0.332	4.64	0.510	7.15	0.179	2 1/2	0.18	1.07	0.25	0.286	4	0.286	
1	1.315	11.5	0.0696	1.2299	0.261	3	0.422	4.85	0.639	7.35	0.217	2 1/2	0.22	1.34	0.30	0.348	4	0.348	
1 1/4	1.660	11.5	0.0696	1.5734	0.261	3	0.446	5.13	0.707	8.13	0.261	3	0.26	1.68	0.39	0.348	4	0.348	
1 1/2	1.900	11.5	0.0696	1.8124	0.261	3	0.463	5.32	0.724	8.33	0.261	3	0.26	1.92	0.43	0.348	4	0.348	
2	2.375	11.5	0.0696	2.2853	0.261	3	0.496	5.70	0.757	8.70	0.261	3	0.26	2.40	0.43	0.348	4	0.348	
2 1/2	2.875	8	0.1000	2.7508	0.500	4	0.638	5.10	1.013	8.10	0.375	3	0.38	2.90	0.63	0.625	5	0.625	
3	3.500	8	0.1000	3.3719	0.500	4	0.700	5.60	1.075	8.60	0.375	3	0.38	3.53	0.63	0.625	5	0.625	
3 1/2	4.000	8	0.1000	3.8688	0.500	4	0.750	6.00	1.125	9.00	0.375	3	0.38	4.04	0.63	0.625	5	0.625	
4	4.500	8	0.1000	4.3656	0.500	4	0.800	6.40	1.175	9.40	0.375	3	0.38	4.54	0.63	0.625	5	0.625	

NOTES:

- (1) These dimensions agree with those developed by the Manufacturers Standardization Society of the Valve and Fittings Industry. Thread lengths are specified to three decimal places for convenience.
- (2) American National Standard Taper Pipe Thread Plug Gage. See Section 7.

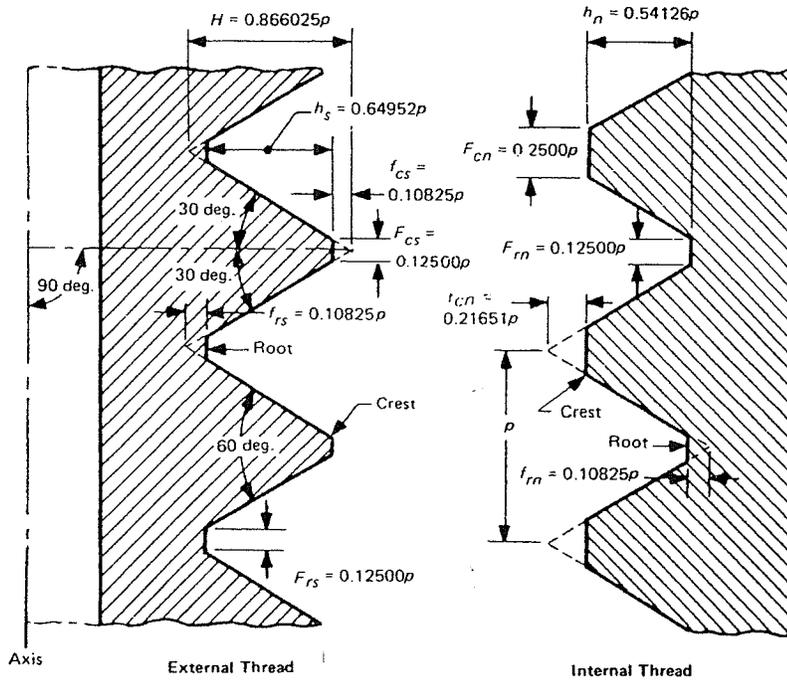


TABLE 6 DIMENSIONS OF EXTERNAL AND INTERNAL STRAIGHT PIPE THREADS FOR FIXTURES, NPSM  
(Free Fitting Mechanical Joints)

Nom. Pipe Size	O.D. of Pipe (D)	Threads/in.	Allowance	External Thread, Class 2A				Internal Thread, Class 2B			
				Major Diameter		Pitch Diameter		Minor Diameter		Pitch Diameter	
				Maximum	Minimum	Maximum	Minimum	Minimum	Maximum	Minimum <sup>1</sup>	Maximum
1	2	3	4	5	6	7	8	9	10	11	12
1/8	0.405	27	0.0011	0.397	0.390	0.3725	0.3689	0.358	0.364	0.3736	0.3783
1/4	0.540	18	0.0013	0.526	0.517	0.4903	0.4859	0.468	0.481	0.4916	0.4974
3/8	0.675	18	0.0014	0.662	0.653	0.6256	0.6211	0.603	0.612	0.6270	0.6329
1/2	0.840	14	0.0015	0.823	0.813	0.7769	0.7718	0.747	0.759	0.7784	0.7851
3/4	1.050	14	0.0016	1.034	1.024	0.9873	0.9820	0.958	0.970	0.9889	0.9958
1	1.315	11.5	0.0017	1.293	1.281	1.2369	1.2311	1.201	1.211	1.2386	1.2462
1 1/4	1.660	11.5	0.0018	1.638	1.626	1.5816	1.5756	1.546	1.555	1.5834	1.5912
1 1/2	1.900	11.5	0.0018	1.877	1.865	1.8205	1.8144	1.785	1.794	1.8223	1.8302
2	2.375	11.5	0.0019	2.351	2.339	2.2944	2.2882	2.259	2.268	2.2963	2.3044
2 1/2	2.875	8	0.0022	2.841	2.826	2.7600	2.7526	2.708	2.727	2.7622	2.7720
3	3.500	8	0.0023	3.467	3.452	3.3862	3.3786	3.334	3.353	3.3885	3.3984
3 1/2	4.000	8	0.0023	3.968	3.953	3.8865	3.8788	3.835	3.848	3.8888	3.8988
4	4.500	8	0.0023	4.466	4.451	4.3848	4.3771	4.333	4.346	4.3871	4.3971
5	5.563	8	0.0024	5.528	5.513	5.4469	5.4390	5.395	5.408	5.4493	5.4598
6	6.625	8	0.0024	6.585	6.570	6.5036	6.4955	6.452	6.464	6.5060	6.5165

GENERAL NOTES:

- (a) NPSM threads are of Unified screw thread form to Classes 2A/2B tolerances, having the minimum pitch diameter of the internal thread basic and equal to  $E_1$  of NPT threads.
- (b) The minor diameters of external threads and major diameters of internal threads are those as produced by commercial straight pipe dies and commercial ground straight pipe taps.  
The major diameter of the external thread has been calculated on the basis of a truncation of  $0.10825p$ , and the minor diameter of the internal thread has been calculated on the basis of a truncation of  $0.21651p$ , to provide no interference at crest and root when product is gaged with gages made in accordance with 9.2.

NOTE:

- (1) Column 11 is the same as the pitch diameter at the large end of internal thread,  $E_1$ , Basic. (See Table 2, col. 8.)

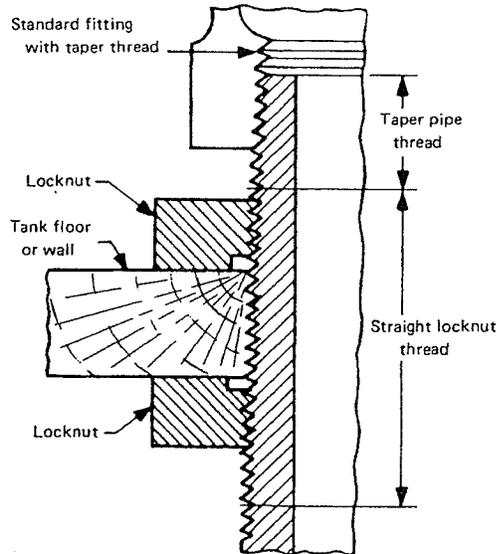


TABLE 7 DIMENSIONS, EXTERNAL AND INTERNAL STRAIGHT PIPE THREAD FOR LOCKNUT CONNECTIONS, NPSL (Loose Fitting Mechanical Joints)

Nominal Pipe Size	O.D. of Pipe (D)	Threads/inch	External Threads			Internal Threads		
			Maximum <sup>1</sup> Major Diameter	Pitch Diameter		Minimum <sup>1</sup> Minor Diameter	Pitch Diameter	
				Maximum	Minimum		Minimum	Maximum
1	2	3	4	5	6	7	8	9
1/8	0.405	27	0.409	0.3840	0.3805	0.362	0.3863	0.3898
1/4	0.540	18	0.541	0.5038	0.4986	0.470	0.5073	0.5125
3/8	0.675	18	0.678	0.6409	0.6357	0.607	0.6444	0.6496
1/2	0.840	14	0.844	0.7963	0.7896	0.753	0.8008	0.8075
3/4	1.050	14	1.054	1.0067	1.0000	0.964	1.0112	1.0179
1	1.315	11.5	1.318	1.2604	1.2523	1.208	1.2658	1.2739
1 1/4	1.660	11.5	1.663	1.6051	1.5970	1.553	1.6106	1.6187
1 1/2	1.900	11.5	1.902	1.8441	1.8360	1.792	1.8495	1.8576
2	2.375	11.5	2.376	2.3180	2.3099	2.265	2.3234	2.3315
2 1/2	2.875	8	2.877	2.7934	2.7817	2.718	2.8012	2.8129
3	3.500	8	3.503	3.4198	3.4081	3.344	3.4276	3.4393
3 1/2	4.000	8	4.003	3.9201	3.9084	3.845	3.9279	3.9396
4	4.500	8	4.502	4.4184	4.4067	4.343	4.4262	4.4379
5	5.563	8	5.564	5.4805	5.4688	5.405	5.4884	5.5001
6	6.625	8	6.620	6.5372	6.5255	6.462	6.5450	6.5567
8	8.625	8	8.615	8.5313	8.5196	8.456	8.5391	8.5508
10	10.750	8	10.735	10.6522	10.6405	10.577	10.6600	10.6717
12	12.750	8	12.732	12.6491	12.6374	12.574	12.6569	12.6686

NOTE:

(1) NPSL threads are standard pipe thread form where the pitch diameters of the external threads are fixed at 2.5 and 4 turns larger than basic  $E_1$ , and where the pitch diameters of the internal threads are fixed at 5 and 6.5 turns larger than basic  $E_1$ , thus providing an allowance equivalent to one turn of the standard taper pipe thread.

As the American National Standard Straight Pipe Thread form of thread is produced by a single tool, the major and the minor diameters of the internal thread and the minor diameter of the external thread are presumed to vary with the pitch diameter. The major diameter of the external thread is usually determined by the diameter of the pipe. These theoretical diameters result from adding the depth of the truncated thread ( $0.666025 \times p$ ) to the maximum pitch diameters in col. 5, and it should be understood that commercial pipe will not always have these maximum major diameters.

The locknut thread is established on the basis of retaining the greatest possible amount of metal thickness between the bottom of the thread and the inside of the pipe.

In order that a locknut may fit loosely on the externally threaded part, an allowance equal to the increase in pitch diameter per turn is provided, with a tolerance of 1.5 turns for both external and internal threads.

larger end of the pipe thread. See Table 5. The dimensions of these external and internal threads are shown in Table 5. A recess in the fitting provides a covering for the last scratch or sharp edges of incomplete threads on the pipe.

**5.1.1 Thread Designation.** American National Standard Railing Joint Taper Pipe Threads are designated in accordance with 1.2.1 as follows:

1/2 - 14 NPTR

**5.1.2 Form of Thread.** The form of the thread is the same as the form of the American National Standard Taper Pipe Thread shown in Fig. 1.

**5.1.3 Tolerances on Thread Elements.** The gaging of these threads is specified in Table 5. The maximum allowable deviation in the external thread is no turns large and one turn small. The maximum allowable deviation in the internal thread is one turn large, no turns small.

## 6 SPECIFICATIONS FOR STRAIGHT PIPE THREADS FOR MECHANICAL JOINTS; NPSM, NPSL, NPSH

### 6.1 Straight Pipe Threads

In addition to pressure-tight pipe joints, for which taper external threads and either taper or straight internal threads are used, there are mechanical joints where straight pipe threads are used to advantage on both external and internal threads. Three of these straight pipe thread joints are covered by this Standard, all of which are based on the pitch diameter of the American National Standard Taper Pipe Thread at the gaging notch (dimension  $E_1$  of Table 2) but have various truncations at crest and root as described below. These three types of joints are as follows:

(a) free-fitting mechanical joints for fixtures, Table 6, both external and internal, NPSM.

(b) loose-fitting mechanical joints with locknuts, Table 7, both external and internal, NPSL.

(c) loose-fitting mechanical joints for hose couplings (ANSI B2.4), NPSH.

**6.1.1 Thread Designations.** The above types of straight pipe threads for mechanical joints are designated in accordance with 1.2.1 as follows:

1/8 - 27 NPSM

1/8 - 27 NPSL

1 - 11.5 NPSH

**6.1.2 Pitch and Flank Angle.** The pitch and flank angle are the same as the corresponding dimensions of the taper pipe thread described in Section 3.

**6.1.3 Diameter of Thread.** The basic pitch diameter for both the external and internal straight pipe threads is equal to the pitch diameter of the American National Standard Taper Pipe Thread at the gaging notch (dimension  $E_1$  of Table 2), which is the same as at the large end of the internal taper pipe thread.

### 6.2 Free-Fitting Mechanical Joints for Fixtures, NPSM

Pipe is often used for special applications where there are no internal pressures. Where straight thread joints are required for mechanical assemblies, straight pipe threads are often found more suited or convenient.

The dimensions of these threads, as given in Table 6, are for pipe thread connections where reasonably close fit of the mating parts is desired.

### 6.3 Loose-Fitting Mechanical Joints With Locknuts, NPSL

The American National Standard External Locknut thread is designed to produce a pipe thread having the largest diameter that it is possible to cut on standard pipe. Ordinarily Straight Internal Threads are used with these Straight External Threads, providing a loose fit. The dimensions of these threads are given in Table 7. It will be noted that the maximum major diameter of the external thread is slightly greater than the nominal outside diameter of the pipe. The normal manufacturer's variation in pipe diameter provides for this increase.

One application of a taper pipe thread in combination with a locknut thread which has been in use for some time is that shown in Table 7. It consists of the nipple threaded joint used to connect standpipes with the floor or wall of a water supply tank.

Gaging information for these threads is given in Section 7.

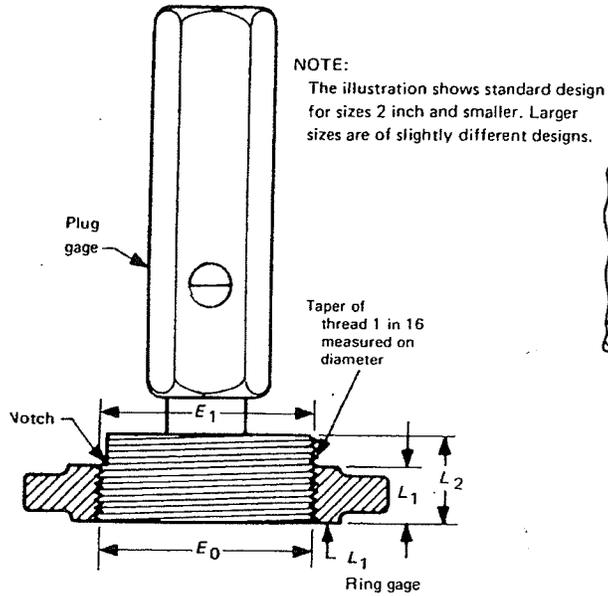


FIG. 4 NPT STANDARD TAPER PIPE THREAD  
PLUG AND RING GAGES

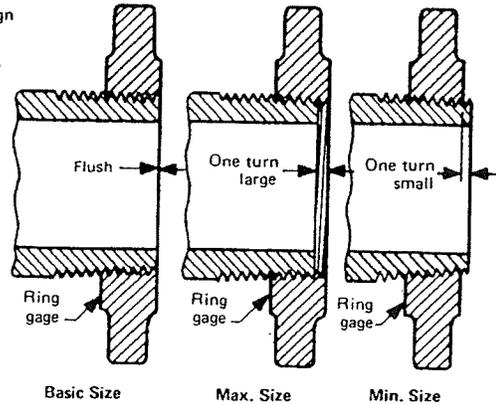


FIG. 6 GAGING EXTERNAL TAPER THREADS  
WITH RING GAGE

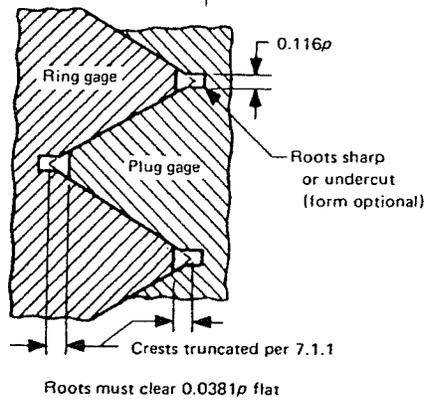


FIG. 5 SUGGESTED FORM OF GAGE THREAD

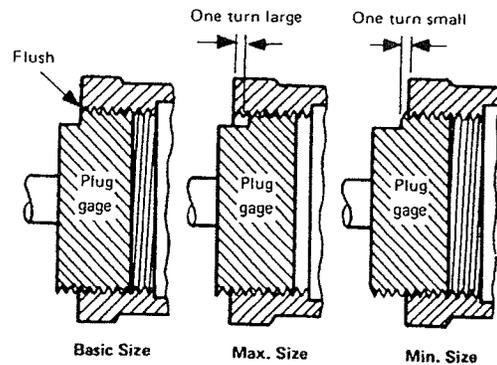
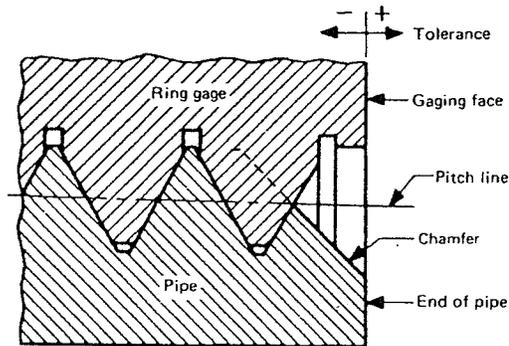
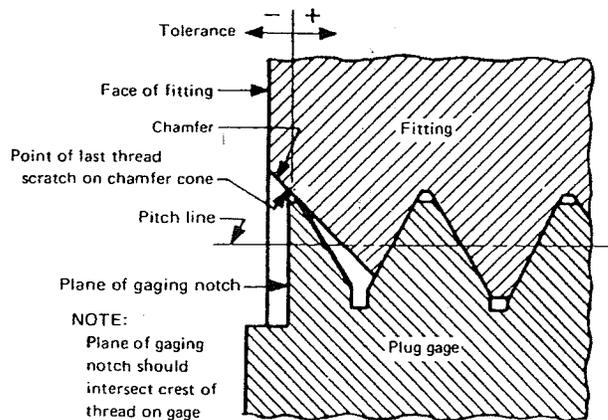


FIG. 7 GAGING INTERNAL TAPER THREADS



(A) Enlarged view showing chamfered external thread of basic size



(B) Enlarged view showing chamfered internal thread of basic size with chamfer exceeding the major diameter

**GENERAL NOTE:**

The chamfer illustrated is at 45 deg. angle and is approximately  $\frac{1}{2}$  pitch in depth. However, these details are not requirements and are given only for information on the illustration shown. The chamfered portion of thread and the full chamfer cone are indicated by dotted lines.

The reference point for the internal product thread is the starting end of the fitting, providing the chamfer does not exceed the major diameter of the internal thread. When a chamfer on the product thread exceeds this limit, the reference point becomes the last thread scratch on the chamfer cone, as illustrated. Allowance must be made for depth of counterbore on counterbored fittings.

**FIG. 8 GAGING OF CHAMFERED THREADS**  
(See 8.4)



#### 6.4 Loose-Fitting Mechanical Joints for Hose Couplings, NPSH

Hose coupling joints are ordinarily made with straight internal and external loose-fitting threads. There are several standards of hose threads having various diameters and pitches, one of which is based on the American National Standard Pipe Thread. By the use of this thread series, it is possible to join small hose couplings in sizes  $\frac{1}{2}$  to 4, inclusive, to ends of standard pipe having American National Standard External Pipe Threads, using a gasket to seal the joint. For dimensions and tolerances, see ANSI B2.4.

### 7 GAGES AND GAGE TOLERANCES FOR AMERICAN NATIONAL STANDARD PIPE THREADS

#### 7.1 Design of Gages

Gages for American National Standard Pipe Threads provide a functional check and are of the standard type as described below. Gages should conform to the designs recommended in ANSI Standard B47.1, Gage Blanks.

**7.1.1 Standard Type Gages.** A set of standard or basic type gages consists of a taper-threaded plug gage and a taper-threaded ring gage. See Figs. 4 and 5. The plug gages are made to dimensions given in Table 8 with a gaging notch located a distance  $L_1$  from the small end. The  $L_1$  ring gage has a length equal to dimension  $L_1$ . The roots of the threads on these gages shall clear  $0.0381p$  width. A sharp  $V$  or undercut clearance is acceptable. The crests are to be truncated an amount equal to  $0.140p$  for 27 threads per inch (tpi),  $0.109p$  for 18 tpi, and  $0.100p$  for 14 tpi, 11-1/2 tpi and 8 tpi threads (see Fig. 5). In locating the basic gaging notch, the plane of the notch should intersect the crest of the gage thread.

The ring gage shall be fitted to the plug so that, when assembled handtight, the gaging notch of the plug gage will be flush with the large end face of the ring gage within tolerances as given in Table 9.

Partial end threads shall be removed on both ends of the ring gage and on the small end of the plug gage to full-form profile in order to avoid possible seating error from bent or malformed feathered edge.

**7.1.2 Marking of Gages.** Each gage shall be marked so as to indicate clearly the nominal size of pipe,

threads per inch, and the proper thread series designation as given in the respective section of this Standard.

#### 7.2 Classes of Gages

Gages of the following types may be used to completely cover gage requirements:

- (a) master gages used to check working gages.
- (b) working gages used to check threads during manufacture and for conformance inspection.

**7.2.1 Master Gages.** The set of master gages consists of an  $L_1$  taper threaded plug gage and an  $L_1$  taper threaded ring gage (see Figs. 4 and 5). The plug gage is made to dimensions specified in Table 8. It is constructed of hardened steel with a gaging notch located a distance  $L_1$  (Table 2) from the small end. The ring gage has a length equal to dimension  $L_1$  specified in Table 8. This ring is fitted to its mating plug - seating flush at the notch within  $\pm 0.002$  in. for sizes  $1/16$  through 2, within  $\pm 0.003$  in. for sizes 2-1/2 through 12, and within  $\pm 0.005$  in. for sizes 14 and larger. The roots of the threads on these ring gages shall clear a  $0.0381p$  flat or may be undercut beyond a sharp  $V$ . The crests of the plug and ring gage are truncated  $0.100p$ . The set of master gages is used for checking working gages (see 7.3.2). A supplementary check by optical means should be made of flank angle and form.

**CAUTION:** It should be understood that only a specifically matched set of masters ( $L_1$  plug and  $L_1$  ring) can be expected to mate with each other within the tolerance specified. There are many characteristics or deviations in gage elements that may combine to cause a significant standoff difference between master gages which are not specifically matched.

**7.2.2 Working Gages.** Each set of working gages consists of an  $L_1$  taper threaded plug gage and an  $L_1$  taper threaded ring gage and is used for checking the product. These gages are made of hardened steel or equivalent material to dimensions given in Table 8. (See 7.3.2 for tolerance.) In locating the basic notch of the plug gage the plane of the notch should intersect the crest of the thread.

It is to be noted that these gages are truncated at the crest so that they bear only on the flanks of the thread. Thus, although they do not check the crest or root truncations specified in Table 1, they are a satisfactory functional check for the general run of product. When it is deemed necessary to determine

TABLE 8 BASIC DIMENSIONS OF THREADED PLUG AND RING GAGES FOR  
NATIONAL AMERICAN NATIONAL STANDARD TAPER PIPE THREADS, NPT

Nominal Pipe Size	O.D. of Pipe (D)	Threads/ in. (n)	Pitch (p)	Major Diameters of Plug Gages				Pitch Diameters of Plug and Ring Gages				Minor Diameters of Ring Gages			Increase in Diam./ Thread (0.0625/ n)	Thick- ness of Ring (L <sub>1</sub> )
				At Small End Plane (E <sub>0</sub> )	At Gaging Notch Plane (E <sub>1</sub> )	At Large End Plane (E <sub>2</sub> )	At Small End (E <sub>0</sub> )	At Gaging Notch (E <sub>1</sub> )	At Large Plug Gage (E <sub>2</sub> )	At Small End, (E <sub>0</sub> ) Plane	At Gaging Notch (E <sub>1</sub> ) Plane	At Large Notch (E <sub>2</sub> ) Plane				
1		27	0.03704	0.29289	0.30289	0.30921	0.27118	0.28118	0.28750	0.24947	0.25947	0.00231	0.160			
1/16	0.3125	27	0.03704	0.38522	0.39531	0.40171	0.36351	0.37360	0.38000	0.34180	0.35189	0.00231	0.1615			
1/8	0.405	18	0.05556	0.51339	0.52763	0.53850	0.47739	0.49163	0.50250	0.44139	0.45563	0.00347	0.2278			
3/16	0.675	18	0.05556	0.64801	0.66301	0.67350	0.61201	0.62701	0.63750	0.57601	0.59101	0.00347	0.240			
1/2	0.840	14	0.07143	0.80600	0.82600	0.83936	0.75843	0.77843	0.79179	0.71086	0.73086	0.00446	0.320			
3/4	1.050	14	0.07143	1.01525	1.03644	1.04936	0.96768	0.98887	1.00179	0.92011	0.94129	0.00446	0.339			
1	1.315	11.5	0.08696	1.27154	1.29654	1.31422	1.21363	1.23863	1.25630	1.15572	1.18072	0.00543	0.400			
1/4	1.660	11.5	0.08696	1.61504	1.64129	1.65922	1.5713	1.59338	1.60130	1.49922	1.52547	0.00543	0.420			
1/2	1.900	11.5	0.08696	1.85400	1.88025	1.89922	1.79609	1.82234	1.84130	1.73817	1.76442	0.00543	0.420			
2	2.375	11.5	0.08696	2.32693	2.35418	2.37422	2.26902	2.29627	2.31630	2.21111	2.23836	0.00543	0.436			
2 1/2	2.875	8	0.12500	2.80278	2.84541	2.87388	2.71953	2.76216	2.79062	2.63628	2.67891	0.00781	0.682			
3	3.500	8	0.12500	3.42388	3.47175	3.49888	3.34062	3.38850	3.41562	3.25737	3.30525	0.00781	0.766			
3 1/2	4.000	8	0.12500	3.92075	3.97207	3.99888	3.83750	3.88881	3.91562	3.75425	3.80556	0.00781	0.821			
4	4.500	8	0.12500	4.41762	4.47038	4.49888	4.33438	4.38712	4.41562	4.25112	4.30387	0.00781	0.844			
5	5.563	8	0.12500	5.47398	5.53255	5.56188	5.39073	5.44929	5.47862	5.30748	5.36604	0.00781	0.937			
6	6.625	8	0.12500	6.52935	6.59222	6.62388	6.44609	6.50597	6.54062	6.36284	6.42272	0.00781	0.958			
8	8.625	8	0.12500	8.51685	8.58328	8.62388	8.43359	8.50003	8.54062	8.35034	8.41678	0.00781	1.063			
10	10.750	8	0.12500	10.62857	10.70419	10.74888	10.54531	10.62094	10.66562	10.46206	10.53768	0.00781	1.210			
12	12.750	8	0.12500	12.61607	12.70107	12.74888	12.55281	12.61781	12.66562	12.44956	12.53456	0.00781	1.360			
14 O.D.	14.000	8	0.12500	13.85825	13.95588	13.99888	13.77500	13.87262	13.91562	13.69175	13.78937	0.00781	1.562			
16 O.D.	16.000	8	0.12500	15.84575	15.95900	15.99888	15.76250	15.87575	15.91562	15.67925	15.79250	0.00781	1.812			
18 O.D.	18.000	8	0.12500	17.83325	17.95825	17.99888	17.75000	17.87500	17.91562	17.66675	17.79175	0.00781	2.000			
20 O.D.	20.000	8	0.12500	19.82075	19.95357	19.99888	19.73750	19.87031	19.91562	19.65425	19.78706	0.00781	2.125			
24 O.D.	24.000	8	0.12500	23.79575	23.94419	23.99888	23.71250	23.86094	23.91562	23.62925	23.77768	0.00781	2.375			

GENERAL NOTE: Gage blanks shall conform to dimensions given in ANSI B47.1. The major diameters of the plug gages and the minor diameters of the ring gages are based upon the truncations specified in 7.1.1.

whether or not such truncations are within the limits specified, or particularly to see that maximum truncation is not exceeded, it is necessary to make further inspection. For this inspection, optics or optical projection is suggested.

### 7.3 Gage Tolerances

In the manufacture of gages, variations from basic dimensions are unavoidable. Furthermore, gages will wear in use. In order to fix the maximum allowable variations of gages, tolerances have been established. See Table 9 and 7.3.2.

**7.3.1 Master Gage Tolerances.** The set of master gages should be made to the basic dimensions as accurately as possible, but in no case shall the cumulative deviation exceed one-half of the total cumulative tolerance specified in cols. 13 and 14 of Table 9. Each master gage should be accompanied by a record of the measurements of all elements of the thread and the standoff of master plug to master ring (large end of ring gage to basic notch of plug gage).

**7.3.2 Working Gage Tolerances.** All gages applied to the product thread, whether in manufacture or inspection, are designated as working gages. All working gages should be made to the basic dimensions specified in Table 8 and within tolerances specified in Table 9. The maximum wear on a working gage shall not be more than the equivalent of one-quarter turn from its original dimensions.

### 7.4 Relation of Lead and Angle Deviations to Pitch Diameter Tolerances of Gages

When it is necessary to compute from measurements the decimal part of a turn that a gage varies from the basic dimensions, Tables 10 and 11 should be used. Table 10 gives the correction in diameter for angle deviations and Table 11 gives the correction in diameter for lead deviations. These corrections are always added to the pitch diameter in the case of external threads and subtracted in the case of internal threads regardless of whether the lead or angle deviations are either plus or minus.

The diameter equivalent for lead and angle deviations plus the pitch diameter deviation multiplied by 16 gives the longitudinal deviation from basic at the gaging notch. This longitudinal deviation divided by the pitch equals the decimal part of a turn that the gage varies from basic at the gaging notch.

## 8 GAGING OF TAPER PIPE THREADS

### 8.1 Gaging External Taper Threads

In gaging external taper threads, the  $L_1$  ring gage, Fig. 6, is screwed handtight on the pipe or external thread. The thread is within the permissible tolerance when the gaging face of the working ring gage is not more than one turn, large or small, from being flush with the end of the thread, as indicated in Fig. 6.

### 8.2 Gaging Internal Taper Threads

In gaging internal taper threads, the  $L_1$  plug gage, Fig. 4, is screwed handtight into the fitting or coupling. The thread is within the permissible tolerance when the gaging notch of the working plug gage is not more than 1 turn, large or small, from being flush with the end of the thread, as indicated in Fig. 7.

### 8.3 Gaging Practice

**8.3.1 Precautions.** In gaging pipe threads it is common practice to tap or rap the part to assure proper seating of the gage in or on the product thread. However, it is first necessary to clean both the gage and the product threads so that they are free of chips, burrs, abrasives, or other foreign materials.

**8.3.2 Supplemental Gaging.** Gaging of both internal and external threads by use of the  $L_1$  plug and ring gages, illustrated by Figs. 6 and 7, serves to assure conformance to the  $L_1$  elements of the design dimensions. However, conformance to this Standard requires that all basic design dimensions be met within applicable tolerances including extension of the thread elements to provide for wrench-tight make-up. Therefore, in controlling manufacturing practices or as otherwise required, additional methods of measuring or gaging may be employed to supplement  $L_1$  gaging.

### 8.4 Gaging Chamfered, Countersunk, or Recessed Threads

The reference point for gaging internal product threads depends upon the chamfer diameter. When the internal chamfer diameter exceeds the major diameter of the internal thread, the reference point is the last thread scratch on the chamfer cone. See Fig. 8B. Otherwise, when the internal chamfer diameter does not exceed the major diameter of the internal thread, the reference point is the end of the



TABLE 9 TOLERANCES FOR AMERICAN NATIONAL STANDARD WORKING TAPER PIPE THREAD PLUG AND RING GAGES, NPT

Nominal Pipe Size	O.D. of Pipe, (D)	Threads/in.	Tolerance on Pitch Diam., <sup>1</sup>		Tolerance on Lead, <sup>2,4</sup>		Tolerance on Half Angle, <sup>3</sup> Minutes		Tolerance on Taper, <sup>5</sup>		Tolerance on Major Diam.		Tolerance on Minor Diam.		Total Cumulative Tolerances on Pitch Diam.		Standoff between Plug and Ring Gages at Gaging Notch for Dimensions at Opposite Extreme Tolerance Limits <sup>6</sup>
			(±)	(±)	Plugs (±)	Rings (±)	Plugs (+)	Rings (-)	Plugs (-)	Rings (+)	Plugs (+)	Rings (-)	Plugs	Rings	Plugs	Rings	
1	2	3	0.002	0.002	0.002	0.003	15	20	0.0003	0.0006	0.0004	0.0004	0.00080	0.00118	0.00080	0.00118	0.032
1/16	0.3125	27	0.002	0.002	0.002	0.003	15	20	0.0003	0.0006	0.0004	0.0004	0.00080	0.00118	0.00080	0.00118	0.032
1/8	0.405	27	0.002	0.002	0.002	0.003	15	20	0.0003	0.0006	0.0004	0.0004	0.00080	0.00118	0.00080	0.00118	0.032
3/16	0.540	18	0.002	0.002	0.002	0.003	15	20	0.0004	0.0007	0.0006	0.0006	0.00092	0.00134	0.00092	0.00134	0.036
1/4	0.675	18	0.002	0.002	0.002	0.003	15	20	0.0004	0.0007	0.0006	0.0006	0.00092	0.00134	0.00092	0.00134	0.036
5/16	0.840	14	0.003	0.002	0.002	0.003	10	15	0.0006	0.0009	0.0010	0.0010	0.00097	0.00142	0.00097	0.00142	0.038
3/8	1.050	14	0.003	0.002	0.002	0.003	10	15	0.0006	0.0009	0.0010	0.0010	0.00097	0.00142	0.00097	0.00142	0.038
1	1.315	11.5	0.003	0.003	0.003	0.004	10	15	0.0008	0.0012	0.0010	0.0010	0.00121	0.00170	0.00121	0.00170	0.047
1/4	1.660	11.5	0.003	0.003	0.003	0.004	10	15	0.0008	0.0012	0.0010	0.0010	0.00121	0.00170	0.00121	0.00170	0.047
1/2	1.900	11.5	0.003	0.003	0.003	0.004	10	15	0.0008	0.0012	0.0010	0.0010	0.00121	0.00170	0.00121	0.00170	0.047
2	2.375	11.5	0.003	0.003	0.003	0.004	10	15	0.0008	0.0012	0.0010	0.0010	0.00121	0.00170	0.00121	0.00170	0.047
2 1/2	2.875	8	0.005	0.004	0.004	0.005	7	10	0.0010	0.0014	0.0016	0.0016	0.00158	0.00211	0.00158	0.00211	0.059
3	3.500	8	0.005	0.004	0.004	0.005	7	10	0.0010	0.0014	0.0016	0.0016	0.00158	0.00211	0.00158	0.00211	0.059
3 1/2	4.000	8	0.005	0.004	0.004	0.005	7	10	0.0010	0.0014	0.0016	0.0016	0.00158	0.00211	0.00158	0.00211	0.059
4	4.500	8	0.005	0.004	0.004	0.005	7	10	0.0010	0.0014	0.0016	0.0016	0.00158	0.00211	0.00158	0.00211	0.059
5	5.563	8	0.005	0.004	0.004	0.005	7	10	0.0010	0.0014	0.0016	0.0016	0.00158	0.00211	0.00158	0.00211	0.059
6	6.625	8	0.005	0.004	0.004	0.005	7	10	0.0010	0.0014	0.0016	0.0016	0.00158	0.00211	0.00158	0.00211	0.059
8	8.625	8	0.005	0.004	0.004	0.005	7	10	0.0010	0.0014	0.0016	0.0016	0.00158	0.00211	0.00158	0.00211	0.059
10	10.750	8	0.005	0.004	0.004	0.005	7	10	0.0010	0.0014	0.0016	0.0016	0.00158	0.00211	0.00158	0.00211	0.059
12	12.750	8	0.005	0.004	0.004	0.005	7	10	0.0010	0.0014	0.0016	0.0016	0.00158	0.00211	0.00158	0.00211	0.059
14 O.D.	14.000	8	0.008	0.005	0.005	0.006	7	10	0.0010	0.0014	0.0030	0.0030	0.00206	0.00271	0.00206	0.00271	0.076
16 O.D.	16.000	8	0.008	0.005	0.005	0.006	7	10	0.0010	0.0014	0.0030	0.0030	0.00206	0.00271	0.00206	0.00271	0.076
18 O.D.	18.000	8	0.008	0.005	0.005	0.006	7	10	0.0010	0.0014	0.0030	0.0030	0.00206	0.00271	0.00206	0.00271	0.076
20 O.D.	20.000	8	0.008	0.005	0.005	0.006	7	10	0.0010	0.0014	0.0030	0.0030	0.00206	0.00271	0.00206	0.00271	0.076
24 O.D.	24.000	8	0.008	0.005	0.005	0.006	7	10	0.0010	0.0014	0.0030	0.0030	0.00206	0.00271	0.00206	0.00271	0.076

GENERAL NOTES:

- (a) The large end of the master ring gage shall be flush with the gaging notch of its master plug when assembled handtight within  $\pm 0.002$  for sizes  $1/16$  to 2 inclusive, within  $\pm 0.003$  for sizes  $2 1/2$  to 12, inclusive, and within  $\pm 0.005$  for sizes 14 and larger.
  - (b) The tolerances for the length  $L_1$  from small end to gaging notch of the plug gaged (Fig. 4) shall be  $+ 0.000$  and  $- 0.001$  for sizes  $1/16$  to 2, inclusive, and  $+ 0.000$  and  $- 0.002$  for sizes  $2 1/2$  and larger.
  - (c) The tolerances for the over-all thread length  $L_2$  of the plug gage (Fig. 4) shall be  $+ 0.050$  and  $- 0.000$  for all sizes.
  - (d) Tolerances for the thickness  $L_1$  of the ring gage (Fig. 4) shall be  $- 0.000$  and  $+ 0.001$  for sizes  $1/16$  to 2, inclusive, and  $- 0.000$  and  $+ 0.002$  for sizes  $2 1/2$  and larger.
- NOTES:
- (1) To be measured at the gaging notch of plug gage.
  - (2) Allowable variation in lead between any two threads in  $L_1$  length of gage (Fig. 4).
  - (3) In solving for the correction in diameter for angle deviations, the average deviation in half angle for the two sides of thread, regardless of their signs should be taken.
  - (4) The lead and taper on plug and ring gages shall be measured along the pitch line omitting the imperfect threads at each end.
  - (5) Allowable variation in taper in  $L_1$  length of gage (Fig. 4).
  - (6) Maximum possible interchange standoff, any ring against any plug other than its master plug, may occur when taper deviations are zero and all other dimensions are at opposite extreme tolerance limits. Average standoff should be well within these maximum limits.

TABLE 10 DIAMETER EQUIVALENT OF DEVIATION<sup>1</sup> IN HALF INCLUDED ANGLE OF  
THREAD FOR TOOLS AND GAGES<sup>3</sup>

Deviation <sup>2</sup> ( $\delta\alpha$ ) Minutes	8 Threads/in.	11.5 Threads/in.	14 Threads/in.	18 Threads/in.	27 Threads/in.
1	2	3	4	5	6
1	0.00006	0.00004	0.00003	0.00002	0.00002
2	0.00011	0.00008	0.00006	0.00005	0.00003
3	0.00017	0.00012	0.00010	0.00007	0.00005
4	0.00022	0.00016	0.00013	0.00010	0.00007
5	0.00028	0.00019	0.00016	0.00012	0.00008
6	0.00034	0.00023	0.00019	0.00015	0.00010
7	0.00039	0.00027	0.00022	0.00017	0.00012
8	0.00045	0.00031	0.00026	0.00020	0.00013
9	0.00050	0.00035	0.00029	0.00022	0.00015
10	0.00056	0.00039	0.00032	0.00025	0.00017
11	0.00062	0.00043	0.00035	0.00027	0.00018
12	0.00067	0.00047	0.00038	0.00030	0.00020
13	0.00073	0.00051	0.00042	0.00032	0.00022
14	0.00078	0.00054	0.00045	0.00035	0.00023
15	0.00084	0.00058	0.00048	0.00037	0.00025
16	0.00089	0.00062	0.00051	0.00040	0.00027
17	0.00095	0.00066	0.00054	0.00042	0.00028
18	0.00101	0.00070	0.00058	0.00045	0.00030
19	0.00106	0.00074	0.00061	0.00047	0.00031
20	0.00112	0.00078	0.00064	0.00050	0.00033
21	0.00117	0.00082	0.00067	0.00052	0.00035
22	0.00123	0.00086	0.00070	0.00055	0.00036
23	0.00129	0.00089	0.00074	0.00057	0.00038
24	0.00134	0.00093	0.00077	0.00060	0.00040
25	0.00140	0.00097	0.00080	0.00062	0.00041
26	0.00145	0.00101	0.00083	0.00065	0.00043
27	0.00151	0.00105	0.00086	0.00067	0.00045
28	0.00157	0.00109	0.00089	0.00070	0.00046
29	0.00162	0.00113	0.00093	0.00072	0.00048
30	0.00168	0.00117	0.00096	0.00075	0.00050
45	0.00252	0.00175	0.00144	0.00112	0.00075
50	0.00336	0.00233	0.00192	0.00149	0.00099

GENERAL NOTE: Values given in inches at 68° F.

NOTES:

- (1) In solving for the diameter equivalent of angle deviations the average deviation in half included angle for the two sides of the thread regardless of their signs should be taken.
- (2) Diameter equivalent =  $0.53812p \tan \delta\alpha$ , where  $\delta\alpha$  = deviation in half included angle of thread expressed in minutes.
- (3) Table is based upon an NPT gage with 0.1p root/crest Truncations with equal half-angle deviations. For other gages with equal truncations, multiply by

$$\frac{0.866p - 2(\text{truncation})}{0.6667p}$$

TABLE 11 DIAMETER EQUIVALENT OF DEVIATION IN LEAD FOR TOOLS AND GAGES<sup>1</sup>

Deviation ( $\delta p$ )	0.00000	0.00001	0.00002	0.00003	0.00004	0.00005	0.00006	0.00007	0.00008	0.00009
1	2	3	4	5	6	7	8	9	10	11
0.00000	0.00000	0.00002	0.00003	0.00005	0.00007	0.00009	0.00010	0.00012	0.00014	0.00016
0.00010	0.00017	0.00019	0.00021	0.00023	0.00024	0.00026	0.00028	0.00029	0.00031	0.00033
0.00020	0.00035	0.00036	0.00038	0.00040	0.00042	0.00043	0.00045	0.00047	0.00048	0.00050
0.00030	0.00052	0.00054	0.00055	0.00057	0.00059	0.00061	0.00062	0.00064	0.00066	0.00068
0.00040	0.00069	0.00071	0.00073	0.00074	0.00076	0.00078	0.00080	0.00081	0.00083	0.00085
0.00050	0.00087	0.00088	0.00090	0.00092	0.00094	0.00095	0.00097	0.00099	0.00100	0.00102
0.00060	0.00104	0.00106	0.00107	0.00109	0.00111	0.00113	0.00114	0.00116	0.00118	0.00120
0.00070	0.00121	0.00123	0.00125	0.00126	0.00128	0.00130	0.00132	0.00133	0.00135	0.00137
0.00080	0.00139	0.00140	0.00142	0.00144	0.00145	0.00147	0.00149	0.00151	0.00152	0.00154
0.00090	0.00156	0.00158	0.00159	0.00161	0.00163	0.00165	0.00166	0.00168	0.00170	0.00171
0.00100	0.00173	0.00175	0.00177	0.00178	0.00180	0.00182	0.00184	0.00185	0.00187	0.00189
0.00110	0.00191	0.00192	0.00194	0.00196	0.00197	0.00199	0.00201	0.00203	0.00204	0.00206
0.00120	0.00208	0.00210	0.00211	0.00213	0.00215	0.00217	0.00218	0.00220	0.00222	0.00223
0.00130	0.00225	0.00227	0.00229	0.00230	0.00232	0.00234	0.00236	0.00237	0.00239	0.00241
0.00140	0.00242	0.00244	0.00246	0.00248	0.00249	0.00251	0.00253	0.00255	0.00256	0.00258
0.00150	0.00260	0.00262	0.00263	0.00265	0.00267	0.00268	0.00270	0.00272	0.00274	0.00275
0.00160	0.00277	0.00279	0.00281	0.00282	0.00284	0.00286	0.00288	0.00289	0.00291	0.00293
0.00170	0.00294	0.00296	0.00298	0.00300	0.00301	0.00303	0.00305	0.00307	0.00308	0.00310
0.00180	0.00312	0.00313	0.00315	0.00317	0.00319	0.00320	0.00322	0.00324	0.00326	0.00327
0.00190	0.00329	0.00331	0.00333	0.00334	0.00336	0.00338	0.00339	0.00341	0.00343	0.00345
0.00200	0.00346	0.00348	0.00350	0.00352	0.00353	0.00355	0.00357	0.00359	0.00360	0.00362

GENERAL NOTE: Values given in inches at 68° F.

NOTE:

(1) Diameter equivalent =  $1.732\delta p$ , where  $\delta p$  = deviation in lead between any two threads.

fitting. An allowance must be made for the depth of counterbore on counterbored fittings.

The reference point for gaging or measuring the length of external product threads is the end of the pipe.

**8.4.1 Turns-Engagement Method of Gaging.** The turns-engagement method of gaging taper threads with plug and ring pipe thread gages, determines that an adequate number of threads is available at hand engagement, thus avoiding possible complications resulting from gage chamfer and product chamfer. See Table 2, col. 7, for the basic number of turns in the absence of chamfers (e.g., 4.32 turns for 27 tpi), the applicable tolerance being plus or minus one turn (or limits 3.32 to 5.32 turns for 27 tpi).

## 9 GAGING OF STRAIGHT PIPE THREADS

### 9.1 Types of Gages

Gages to properly control the production of these straight threads should be either straight GO and HI (Internal) and GO and LO (External) gages or the regular American National Standard Taper Pipe Thread gages as indicated below.

**9.1.1 Use of Straight and Taper Gages.** Straight GO and HI/LO gages should be used for all types of threaded joints where both the external and internal threads are straight. Taper plug gages should be used for the internal threads of all types of mechanical joints where the external thread is tapered and the internal thread is straight. Taper plug gages used for this purpose should be checked periodically by direct measurement.

**9.1.2 Gaging Pressure-tight Joints.** Taper thread gages shall be used to gage straight internal pipe threads forming part of pressure-tight joints where the external thread is tapered.

The plane of the gaging notch on the American National Standard Taper Pipe Thread plug gage shall come flush with the end of the American National Standard Coupling Straight Pipe Thread (NPSC) (Table 4) or flush with the last thread scratch on the chamfer cone if chamfered with an internal chamfer diameter in excess of the major diameter of the internal thread (see Fig. 8B). A tolerance of one and one-half turns large or small to gage shall be allowed.

**CAUTION:** When using a tapered thread plug gage, nonuniformity of gage wear is a particular problem; therefore, taper plug gages used for this application should be checked by direct measurement of thread form and size in addition to checking against a master.

### 9.2 Gage Dimensions

The straight GO and HI plug gages and the straight GO and LO ring gages used for checking mechanical joint threads, Tables 6 and 7, shall be made to the pitch diameter limits specified in the product tables in accordance with standard practice for straight thread gages as outlined in ANSI B1.2, Gages and Gaging for Unified Screw Threads.

The minimum major diameter of the GO thread plug gage shall be equal to the minimum pitch diameter of the internal thread plus an amount equal to  $0.75H$  ( $0.649519p$ ). The maximum major diameter of the HI thread plug gage shall be equal to the maximum pitch diameter of the internal thread plus an amount equal to  $0.50H$  ( $0.433013p$ ).

The maximum minor diameter of the GO thread ring gage shall be equal to the maximum pitch diameter of the external thread minus an amount equal to  $0.50H$  ( $0.433013p$ ). The minimum minor diameter of the LO thread ring gage shall be equal to the minimum pitch diameter of the external thread minus an amount equal to  $0.25H$  ( $0.216506p$ ).

See ANSI B1.2 for further details and tolerances for these straight thread gages.



## APPENDIX

(This Appendix is not part of American National Standard, Pipe Threads, General Purpose (Inch)  
ANSI/ASME B1.20.1-198x, but is included for information purposes only.)

### Suggested Twist Drill Diameters for Drilled Hole Sizes for Pipe Threads

The drill diameters given in Table 1 are the diameters of the standard and stock drills which are the closest to the minimum minor diameters shown in Table 2, col. 24.

They represent the diameters of the holes which would be cut with a twist drill correctly ground when drilling a material without tearing or flow of metal. This is approximately the condition that exists when a correctly sharpened twist drill is cutting a hole in a homogeneous block of cast iron.

When flat drills are used, the width of the cutting edge may have to be adjusted to produce a hole of the required diameter.

When nonferrous metals and other similar materials are to be drilled and tapped, it may be found necessary to use a drill of slightly larger or smaller diameter to produce a hole of a size that will make it possible for the tap to cut an acceptable pipe thread with the required thread height.

It should be understood that this table of twist drill diameters is intended to help only the occasional user of drills in the application of this Standard. When internal pipe threads are produced in larger quantities in a particular type of material and with specially designed machinery it may be found to be more advantageous to use a drill size not given in the table, even one having a nonstandard diameter.

**TABLE A1 SUGGESTED TWIST DRILL DIAMETERS  
(INCHES) FOR DRILLED HOLE SIZES FOR  
PIPE THREADS**

Nom. Pipe Size	O.D. of Pipe (D)	Taper Thread		Straight Pipe Thread (NPS) <sup>2</sup>
		With use of Reamer	Without use of Reamer	
1	2 <sup>1</sup>	3	4	5
$\frac{1}{16}$	0.3125	A 0.234 <sup>1</sup>	C 0.242 <sup>1</sup>	$\frac{1}{4}$ 0.250 <sup>1</sup>
$\frac{1}{8}$	0.405	$\frac{21}{64}$ 0.328 <sup>1</sup>	Q 0.332 <sup>1</sup>	$\frac{1}{32}$ 0.344 <sup>1</sup>
$\frac{1}{4}$	0.540	$\frac{27}{64}$ 0.422 <sup>1</sup>	$\frac{7}{16}$ 0.438 <sup>1</sup>	$\frac{7}{16}$ 0.438 <sup>1</sup>
$\frac{3}{8}$	0.675	$\frac{9}{16}$ 0.562 <sup>1</sup>	$\frac{9}{16}$ 0.562 <sup>1</sup>	$\frac{37}{64}$ 0.578 <sup>1</sup>
$\frac{1}{2}$	0.840	$\frac{11}{16}$ 0.688 <sup>1</sup>	$\frac{45}{64}$ 0.703 <sup>1</sup>	$\frac{23}{32}$ 0.719 <sup>1</sup>
$\frac{3}{4}$	1.050	$\frac{57}{64}$ 0.891 <sup>1</sup>	$\frac{27}{32}$ 0.906 <sup>1</sup>	$\frac{59}{64}$ 0.922 <sup>1</sup>
1	1.315	$\frac{1}{8}$ 1.125 <sup>1</sup>	$\frac{9}{64}$ 1.141 <sup>1</sup>	$\frac{17}{32}$ 1.156 <sup>1</sup>
$1\frac{1}{4}$	1.660	$1\frac{15}{32}$ 1.469	$1\frac{31}{64}$ 1.484	$1\frac{1}{2}$ 1.500
$1\frac{1}{2}$	1.900	$1\frac{45}{64}$ 1.703	$1\frac{23}{32}$ 1.719	$1\frac{3}{4}$ 1.750
2	2.375	$2\frac{11}{64}$ 2.172	$2\frac{7}{16}$ 2.188	$2\frac{1}{32}$ 2.219
$2\frac{1}{2}$	2.875	$2\frac{37}{64}$ 2.578	$2\frac{39}{64}$ 2.609	$2\frac{1}{32}$ 2.656

**GENERAL NOTE:** The use of twist drills of the diameters listed will not assure completely formed threads over the entire  $L_1$  length.

**NOTES:**

- (1) American National Standard twist drill sizes in accordance with ANSI B94.11, applicable to commercial threads only.
- (2) Twist drill diameters for NPSM, NPSL and NPSH threads may be larger to suit the increased internal minor diameters established for these threads. Refer to Tables 6 and 7 in this Standard and Table 3 in ANSI B2.4, Hose Coupling Screw Threads.

## Section 12



U.S. Department  
of Transportation

Pipeline and Hazardous Materials  
Safety Administration

1200 New Jersey Ave., SE  
Washington, DC 20590

JUL 07 2009

Mr. John W. Somerhalder, II  
President  
AGL Resources, Inc.  
Ten Peachtree Place, NE  
Atlanta, GA 30309

**Re: CPF No. 2-2006-3003**

Dear Mr. Somerhalder:

Enclosed is the Final Order issued in the above-referenced case. It makes findings of violation and assesses a civil penalty of \$303,000. The penalty payment terms are set forth in the Final Order. This enforcement action closes automatically upon payment. Your receipt of the Final Order constitutes service of that document under 49 C.F.R. § 190.5.

Thank you for your cooperation in this matter.

Sincerely,

Jeffrey D. Wiese  
Associate Administrator  
for Pipeline Safety

FOR/

Enclosure

cc: David E. Slovensky, Esq.,  
AGL Resources Inc., Ten Peachtree Place NE, Atlanta, Georgia 30309  
Paul Biancardi, Esq., 5818 Beaver Falls Drive, Kingwood, Texas 77345  
Linda Daugherty, Director, Southern Region, PHMSA  
Richard Lonn, Director, Regulatory Compliance, Chattanooga Gas Company

**CERTIFIED MAIL – RETURN RECEIPT REQUESTED [7005-1160 0001 0046 9716]**



and the matter was scheduled for hearing, which was subsequently held on May 11, 2007, in Atlanta, Georgia. An attorney from the Office of Chief Counsel, PHMSA, served as presiding official pursuant to 49 C.F.R. § 190.211(c). After the hearing, Respondent provided a Post-Hearing Closing Argument (Closing), which was further supplemented by letter dated July 18, 2008.<sup>3</sup>

### FINDINGS OF VIOLATION

AGL did not contest the allegations in the Notice that it violated 49 C.F.R. Parts 193 and 199, as follows:

**Item 1:** The Notice alleged that Respondent violated 49 C.F.R. § 193.2503, which states:

**§ 193.2503 Operating procedures.**

Each operator shall follow one or more manuals of written procedures to provide safety in normal operation and in responding to an abnormal operation that would affect safety....

The Notice alleged that on the date of the Incident, Respondent violated § 193.2503 by failing to follow its own written procedures to provide safety in both normal and abnormal operating situations. At the time of the Incident, AGL's written procedures required that all employees wear personal protective equipment (PPE), including flame-retardant coveralls and hood, whenever "a hazardous or potentially hazardous atmospheric condition exist[ed] on a job site..."<sup>4</sup> Mr. Poss, however, was not wearing flame-retardant clothing when he attempted to clear the clogged filter and, as a result, suffered serious injury.<sup>5</sup> The Notice alleged that AGL failed to ensure that Poss followed these company procedures.

In its Response, AGL did not contest this allegation. Accordingly, upon consideration of all of the evidence, I find that AGL violated 49 C.F.R. § 193.2503 by failing to follow its own written procedures to provide safety in normal operation and in responding to an abnormal operation that would affect safety.

**Item 2:** The Notice alleged that Respondent violated 49 C.F.R. § 193.2503(f)(4), which states:

**§ 193.2503 Operating procedures.**

Each operator shall follow one or more manuals of written procedures to provide safety in normal operation and in responding to an abnormal operation that would affect safety. The procedures must include provisions for:

---

<sup>3</sup> AGL confirmed in its Closing that it did not wish to contest the allegation of violation in the Notice. See Closing, 1.

<sup>4</sup> Chattanooga Gas Company Safety Manual, Paragraph 5.3 (1993).

<sup>5</sup> *Investigation Report, supra*, at 2.

- (a) ....
- (f) In the case of liquefaction, maintaining temperatures, pressures, pressure differentials and flow rates, as applicable, within their design limits for:
  - (1) ....
  - (4) Purification and regeneration equipment;....

The Notice alleged that Respondent violated § 193.2503 by failing to follow its own manual of written liquefaction procedures for maintaining pressure differentials and flow rates for purification and regeneration equipment, within their design limits. Specifically, the Notice alleged that AGL failed to follow the instructions in the manufacturer's manual for maintaining pressure differentials across the F-101 filter within its design limits.<sup>6</sup> The manufacturer (Perry Equipment Corporation) warned in its operating instructions that the pressure drop across the filter should never exceed 35 psi or else the filter elements might collapse.

AGL admitted in its Response that the company was aware of this restriction and expected its employees to adhere to it.<sup>7</sup> However, its employees failed to comply with this restriction and allowed the pressure drop across the filter to reach 54 psi before they shut down the liquefaction process. As a consequence, the filter collapsed, causing molecular sieve and dust particles to ignite. In its Response, AGL did not contest this allegation. Accordingly, upon consideration of all the evidence, I find that Respondent violated 49 C.F.R. §193.2503(f)(4) by failing to follow its own written procedures for maintaining pressure differentials for the F-101 filter within the design limits set by the manufacturer.

**Item 3:** The Notice alleged that Respondent violated 49 C.F.R. § 193.2603, which states:

**§ 193.2603 General.**

- (a) Each component in service, including its support system, must be maintained in a condition that is compatible with its operational or safety purpose by repair, replacement, or other means.
- (b) An operator may not place, return, or continue in service any component which is not maintained in accordance with this subpart.

The Notice alleged that AGL violated § 193.2603 by failing to maintain various components of the LNG Plant equipment in a condition that was compatible with their operational or safety purpose by repair, replacement, or other means. Specifically, it alleged that AGL failed to properly maintain the three dehydrator towers. The Notice further noted that Respondent had continued to keep the dehydrators in service despite known problems dating back to 2003.

During the LNG liquefaction pre-treatment process, water, carbon dioxide, and other compounds

<sup>6</sup> The pressure differential for the filter is calculated by subtracting the outlet pressure from the inlet pressure. The inlet pressure is a reading taken from a gauge installed upstream from the dehydrator. The outlet pressure is a reading taken from a gauge installed at the outlet of the cold box.

<sup>7</sup> Closing, at 7.

are removed by using a dehydrator and molecular sieve towers.<sup>8</sup> As revealed by the AGL internal investigation, the caulking that sealed the gap between the mesh and the inside wall of all three towers failed, allowing sieve under pressure to be forced out of the dehydrator and causing the F-101 filter to clog.<sup>9</sup> As explained in the Investigation Report, the F-101 filter had routinely clogged prior to the Incident, becoming blocked by molecular sieve and dust that originated in the dehydrator.<sup>10</sup> Although AGL cleaned and replaced the filter numerous times, it did not repair or replace the dehydrator, the source of the problem. As recently as six days prior to the Incident, the filter clogged and required cleaning. Respondent chose to install an additional strainer to catch the sieve rather than to properly repair the dehydrator but both strainers failed prior to the Incident.

Proper maintenance and repair of these various components could have prevented the May 13, 2005 fire. AGL did not contest this allegation. Accordingly, upon consideration of all of the evidence, I find that Respondent violated 49 C.F.R. § 193.2603 by failing to maintain the dehydrator and other related components in a condition that was compatible with their operational or safety purpose by repair, replacement, or other means.

**Item 4:** The Notice alleged that Respondent violated 49 C.F.R. § 199.105(b), which states:

**§ 199.105 Drug tests required.**

Each operator shall conduct the following drug tests for the presence of a prohibited drug:

(a) ...

(b) *Post-accident testing.* As soon as possible but no later than 32 hours after an accident, an operator shall drug test each employee whose performance either contributed to the accident or cannot be completely discounted as a contributing factor to the accident. An operator may decide not to test under this paragraph but such a decision must be based on the best information available immediately after the accident that the employee's performance could not have contributed to the accident or that, because of the time between that performance and the accident, it is not likely that a drug test would reveal whether the performance was affected by drug use....

The Notice alleged that Respondent violated § 199.105(b) by failing, within 32 hours after an accident, to drug test an employee whose performance either contributed to the accident or could not be completely discounted as a contributing factor. Specifically, the Notice alleged that Respondent failed to drug test within 32 hours the employee who was involved and injured in the Incident. AGL failed either to provide a reasonable explanation for its failure to test or to

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<sup>8</sup> *Investigation Report, supra*, at 7.

<sup>9</sup> *Id.* at 9.

<sup>10</sup> *Id.*

demonstrate that the employee's performance could be completely discounted as a contributing factor to the accident. AGL did not contest this allegation. Accordingly, upon consideration of all of the evidence, I find that Respondent violated 49 C.F.R. § 199.105(b) by failing to drug test, within 32 hours, the employee involved and injured in the Incident.

**Item 5:** The Notice alleged that Respondent violated 49 C.F.R. § 199.225 (a)(1), which states:

**§ 199.225 Alcohol tests required.**

Each operator shall conduct the following types of alcohol tests for the presence of alcohol:

(a) *Post-accident.* (1) As soon as practicable following an accident, each operator shall test each surviving covered employee for alcohol if that employee's performance of a covered function either contributed to the accident or cannot be completely discounted as a contributing factor to the accident. The decision not to administer a test under this section shall be based on the operator's determination, using the best available information at the time of the determination, that the covered employee's performance could not have contributed to the accident.

The Notice alleged that Respondent violated § 199.225(a)(1) by failing to test, as soon as practicable following an accident, each surviving covered employee for alcohol if that employee's performance of a covered function either contributed or could not be completely discounted as a contributing factor to the accident. Specifically, the Notice alleged that AGL failed to test, as soon as practicable, the employee involved and injured in the Incident. Respondent failed either to provide a reasonable explanation for its failure to test or to demonstrate that the employee's performance could not be completely discounted as a contributing factor to the accident. In its Response, AGL did not contest this allegation. Accordingly, upon consideration of all of the evidence, I find that Respondent violated 49 C.F.R. § 199.225(a)(1) by failing to test for alcohol use, as soon as practicable, the employee involved and injured in the Incident.

These findings of violation will be considered prior offenses in any subsequent enforcement action taken against Respondent.

**ASSESSMENT OF PENALTY**

Under 49 U.S.C. § 60122, Respondent is subject to an administrative civil penalty not to exceed \$100,000 per violation for each day of the violation, up to a maximum of \$1,000,000 for any related series of violations.

49 U.S.C. § 60122 and 49 C.F.R. § 190.225 require that, in determining the amount of a civil penalty, I consider the following criteria: the nature, circumstances, and gravity of the violation, including adverse impact on the environment; the degree of Respondent's culpability; the history of Respondent's prior offenses; the Respondent's ability to pay the penalty and any effect that

the penalty may have on its ability to continue doing business; and the good faith of Respondent in attempting to comply with the pipeline safety regulations. In addition, I may consider the economic benefit gained from the violation without any reduction because of subsequent damages, and such other matters as justice may require. The Notice proposed a total civil penalty of \$303,000 for violations of 49 C.F.R. §§ 193.2503, 193.2503(f)(4), 193.2603, 199.105(b), and 199.225(a)(1).

AGL did not contest any of the findings of violation but presented five distinct arguments why the total penalty should be reduced. The first involved the gravity and circumstances of each violation and is therefore discussed separately under each Item below. The other four, which can be discussed collectively, are as follows: (1) that the Incident and injuries were the direct result of employee misconduct rather than the culpability of the company; (2) that AGL had made a substantial good-faith investment after the Incident in certain company-wide safety enhancements; (3) that the company had no history of prior offenses; and (4) that 10 other Final Orders issued by OPS in the past provided for mitigation of a proposed penalty based upon the operator's conduct subsequent to issuance of the Notice.

I find these last four arguments unpersuasive. First, it is well settled that pipeline operators are ultimately responsible for the acts and omissions of their employees, contractors, and agents in complying with federal pipeline safety regulations. Furthermore, such a policy conforms to the traditional doctrine of *respondeat superior* under which AGL is legally responsible for the actions of its employees and agents acting within the scope of their employment. Even if AGL had appropriate safety procedures in place at the time of the Incident, the company still failed to take effective action to ensure that the procedures were actually followed by individuals performing work at the LNG Plant.

In fact, it is troubling that Respondent attempts to shift responsibility and culpability for its own regulatory violations to two front-line employees.<sup>11</sup> An organization with an effective safety culture is one that imposes multiple safety "barriers" to reduce the risks and consequences of accidents. Under Respondent's argument, no pipeline operator that had adopted adequate safety procedures but then failed to monitor or supervise its personnel in carrying them out would ever be held liable for its own regulatory violations. Under the circumstances of this case, it is clear that AGL failed on multiple levels to take the measures necessary to prevent the Incident and to ensure that its employees actually followed company procedures.

Second, AGL argued that its actions after the Incident reflected a sincere, good-faith effort to improve safety conditions at the company and that such efforts should serve to mitigate the proposed penalty. The company stated that it had made "substantial investments in time and money which had yielded demonstrable improvements in the safety of the Company's overall operations."<sup>12</sup> These improvements, it argued, were not limited to ones directly related to the

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<sup>11</sup> For example, AGL states in its Closing: "The Company did not condone or ratify the misconduct of Poss or [Plant Superintendent] Young in failing to follow applicable policies and manufacturer's instructions, and the Company notes that neither individual is presently employed by the Company." Closing at 1.

<sup>12</sup> Closing, at 2.

Incident but encompassed a broad range of measures designed to foster “a renewed safety focus across all operations.” This included a commitment, made prior to issuance of the Notice, to invest more than \$1.77 million on actions that went “above and beyond the requirements of 49 CFR Part 193.”<sup>13</sup>

While such measures may reflect a sincere and effective effort to improve safety, they do not constitute a basis for mitigating a penalty imposed for multiple, significant safety violations that occurred prior to a serious accident. PHMSA has indeed recognized a “good faith” defense for actions voluntarily taken by an operator *before* a violation to achieve regulatory compliance; it has not generally recognized this defense for corrective actions taken in *response* to an accident or enforcement proceeding. In this case, I find that the actions taken by AGL after the Incident were largely ones that any reasonable and prudent operator would have taken to protect its facilities and operating personnel and do not constitute a basis for reducing a penalty.

Third, AGL argued that it had not previously been cited by PHMSA for the specific violations listed in the Notice. While this may be correct, an operator’s history of prior violations is one of several considerations listed in 49 C.F.R. § 190.225 and by which a proposed civil penalty is initially calculated. In this case, AGL’s prior enforcement history was considered by PHMSA in calculating the proposed penalty; otherwise, the proposed penalties might have been substantially higher.

Finally, Respondent’s counsel referred to 10 other OPS Final Orders in which a civil penalty was reduced. As discussed at the hearing and as referenced above, all of the penalty assessment considerations enumerated in 49 U.S.C. § 60122 are evaluated in calculating a proposed penalty. In fairness, this necessarily entails an independent assessment of the totality of the facts and circumstances of each case. This case involved an accident that resulted in one employee being seriously injured and that could have easily resulted in a major catastrophe. Therefore, it is difficult to draw meaningful parallels between this case and the ones cited by Respondent.

In addition to these general arguments, AGL raised the following specific arguments for mitigation of the penalties proposed for Items 1-5:

**Item 1.** The Notice proposed a civil penalty of \$41,000 for Respondent’s violation of 49 C.F.R. § 193.2503, for failing to follow its own written procedures requiring the use of PPE. In its post-hearing submissions, Respondent acknowledged the seriousness of the employee’s injuries but asserted that they were the result of his own “poor choices,” not those of the company.<sup>14</sup> AGL argued that Mr. Poss elected to violate standard AGL procedures by failing to wear the PPE and chose to stand in the flow of gas when cleaning the filter, thus increasing the risk and extent of his injuries. The company also argued that the penalty should reflect the fact that the company had provided Poss with proper training on the company’s safety procedures and the usage of PPE prior to the Incident.

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<sup>13</sup> *Id.*

<sup>14</sup> *Id.* at 4.

I disagree. First, the gravity of this violation cannot be overstated. Not only was Mr. Poss severely injured and hospitalized with second- and third-degree burns, but the consequences of the Incident could easily have been far worse. AGL is fortunate that only one employee was injured and that the fire was quickly contained. Regardless of any mistakes that the employees may have made, the fact remains that Mr. Poss would not have suffered significant injuries if AGL had taken adequate measures to ensure that its personnel properly followed the company's procedures on PPEs. Accordingly, having reviewed the record and considered the assessment criteria, I assess Respondent a civil penalty of \$41,000 for Item 1.

**Item 2.** The Notice proposed a civil penalty of \$91,000 for Respondent's violation of 49 C.F.R. § 193.2503(f)(4), for failing to follow the manufacturer's written instructions for maintaining pressure differentials and flow rates for purification and regeneration equipment within their design limits. As stated above, Respondent admitted that it allowed the pressure drop across the filter to exceed the manufacturer's stated allowance. AGL argued nevertheless that a reduced penalty was appropriate because: (1) AGL was not required by the pipeline safety regulations to maintain equipment to measure the pressure differential across the filter; (2) the violation was a result of employee misconduct; and (3) the fire was quickly controlled and did not present a risk to the public.

I find these arguments unconvincing. First, it is true that Respondent was not required to maintain specific equipment to measure the pressure differential across the filter, but it was required to adopt and follow procedures for "maintaining temperatures, pressures, pressure differentials and flow rates, as applicable, within [the purification and regeneration equipment's] design limits."<sup>15</sup> Although AGL acknowledged that it was aware of the manufacturer's design limits for the filter and attempted to observe the pressure drop by periodically observing the flow, it had a clear responsibility to maintain the proper pressure levels by whatever means necessary. The company failed to do this. Respondent stated that it has since installed a measuring device to detect the pressure drop. However, as explained above, this post-incident action is not persuasive of an operator's good faith in attempting to comply with the pipeline safety regulations prior to an incident.

As noted above, the alleged misconduct of AGL employees does not absolve the company of its own obligation to properly maintain its equipment so that it does not pose a safety risk. Likewise, the fact that the fire was contained and did not result in greater injury does not reduce the culpability of the operator. Accordingly, having reviewed the record and considered the assessment criteria, I assess Respondent a civil penalty of \$91,000 for Item 2.

**Item 3.** The Notice proposed a civil penalty amount of \$131,000 for Respondent's violation of 49 C.F.R. § 193.2603, for failing to maintain the three dehydrator towers. As stated above, I found that the fire and the resulting injuries to Mr. Poss would not have occurred if the liquefaction equipment had been properly maintained. In addition to the general arguments discussed earlier, AGL argued that a reduced penalty was appropriate for this Item because the company had made a good-faith effort, prior to the Incident, to correct the problem with the F-101 filter by installing an additional strainer and replacing the filter.

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<sup>15</sup> 49 C.F.R. § 193.2503.

Even though such measures may have been taken prior to the Incident, I still do not believe they rise to the level of a valid "good faith" defense. Under § 193.2603, operators have an affirmative obligation to maintain their equipment "in a condition that is compatible with its operational or safety purpose by repair, replacement, or other means." AGL had experienced repeated problems with molecular sieve at the LNG plant dating back to 2003 and occurring as recently as six days prior to the Incident. The company clearly knew or should have known that its previous repair efforts had been unsuccessful, that the dehydrator was not operating properly, and that more extensive repairs were necessary in order to comply with the regulation.

Since Respondent failed to repair the dehydrator towers or to fix the underlying cause of the filter problems, despite having had ample opportunities to do so for several years, I find that the proposed penalty of \$131,000 is warranted. Accordingly, having reviewed the record and considered the assessment criteria, I assess Respondent a civil penalty of \$131,000 for Notice Item 3.

**Items 4 and 5.** The Notice proposed a civil penalty of \$40,000 for violation of 49 C.F.R. § 199.105(b) and 49 C.F.R. § 199.225(a)(1), for Respondent's failure to drug and alcohol test the involved employee after the Incident.

Respondent did not provide an explanation for its failure to conduct the drug and alcohol tests, but noted that the employee's supervisor, who was an hour-and-a-half away from the LNG Plant at the time of the Incident, was more focused on managing the incident response and assisting with the hospitalization of the injured employee than with conducting the alcohol and drug tests. While this may be understandable, such is the case for most accidents involving injuries. In addition, § 199.105(b) allows for drug testing to occur within a 32-hour window and § 199.225 (a)(1) requires that alcohol testing occur "as soon as practicable" following an accident.<sup>16</sup> AGL had ample opportunity to meet both requirements. Furthermore, the injured employee was taken to a hospital, where the tests could have readily been performed.

Accordingly, having reviewed the record and considered the assessment criteria, I assess Respondent a civil penalty of \$20,000 for Item 4 and \$20,000 for Item 5.

In summary, having reviewed the record and considered the assessment criteria for all the Items discussed above, I assess Respondent a total civil penalty of **\$303,000**.

Payment of the civil penalty must be made within 20 days of service. Federal regulations (49 C.F.R. § 89.21(b)(3)) require this payment be made by wire transfer, through the Federal Reserve Communications System (Fedwire), to the account of the U.S. Treasury. Detailed instructions are contained in the enclosure. Questions concerning wire transfers should be directed to: Financial Operations Division (AMZ-341), Federal Aviation Administration, Mike Monroney Aeronautical Center, P.O. Box 269039, Oklahoma City, OK 73125; (405) 954-8893.

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<sup>16</sup> §§ 199.105(b) and 199.225(a)(1).

Failure to pay the \$303,000 civil penalty will result in accrual of interest at the current annual rate in accordance with 31 U.S.C. § 3717, 31 C.F.R. § 901.9 and 49 C.F.R. § 89.23. Pursuant to those same authorities, a late penalty charge of six percent (6%) per annum will be charged if payment is not made within 110 days of service. Furthermore, failure to pay the civil penalty may result in referral of the matter to the Attorney General for appropriate action in a United States District Court.

Under 49 C.F.R. § 190.215, Respondent has a right to submit a Petition for Reconsideration of this Final Order. The petition must be received within 20 days of Respondent's receipt of this Final Order and must contain a brief statement of the issue(s). The filing of the petition automatically stays the payment of any civil penalty assessed. However if Respondent submits payment for the civil penalty, the Final Order becomes the final administrative decision and the right to petition for reconsideration is waived. The terms and conditions of this Final Order shall be effective upon receipt.



Jeffrey D. Wiese  
Associate Administrator  
for Pipeline Safety

7/7/09  
Date Issued